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Numerical assessment of wall modelling approaches in scale-resolving in-cylinder simulations

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Abstract

Wall modelling in internal combustion engines (ICEs) is a challenging task due to highly specific boundary layers and a dynamically changing flow environment. Recent experimental (Jainski et al., 2013; Renaud et al., 2018) and direct numerical simulation (DNS, Schmitt et al., 2015a) studies demonstrate that scaled near-wall velocity and temperature profiles in ICEs deviate considerably from the law of the wall. Utilising the DNS data, the present paper focusses on benchmarking a scale-resolving approach with a 1-D non-equilibrium wall model (HLR-WT, Keskinen et al., 2017) in ICE-like flows. Specific emphasis is put on the compression stroke using different grids and two additional wall-modelled large eddy simulation (WMLES) reference approaches. The standard wall law based WMLES-1 produces highly grid-dependent underprediction of wall fluxes, to which WMLES-2 (Plensgaard and Rutland, 2013) and HLR-WT, employing engine-targeted wall treatments, yield considerable improvement. Differences between the improved methods are noted in detailed metrics. Throughout the compression stroke, HLR-WT provides a good match to the DNS in scaled mean boundary layer profiles for both velocity and temperature. With relevance to local heat flux distribution, the characteristic impingement-ejection process observed in the DNS

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is qualitatively replicated with WMLES-2 and HLR-WT. The non-equilibrium formulation of the latter allows for slight improvements in terms of local heat transfer fluctuation predictions. In contrast, coarse near-wall grids appear to be detrimental for such predictions with all approaches. The study provides evidence on the potential of the HLR-WT and WMLES-2 approaches in ICE near-wall flow prediction, advocating further investigations in more realistic engine configurations.

Keywords: Wall modelling, Wall-modelled large eddy simulation, Engine flows, Compression stroke, Wall heat transfer

1. Introduction

1.1. Background

Near-wall fluid flow processes and wall heat transfer have a substantial influence on internal combustion engine (ICE) charge conditions such as temperature and flow turbulence. With the concurrent prospect of high thermal efficiency and low emissions, ICE research and development is increasingly focussed on modern, sensitive concepts such as lean combustion, homogeneous charge compression ignition (HCCI) or reactivity controlled compression ignition (RCCI) (Reitz, 2013). Hence, the understanding and predictive analysis of such modern concepts benefits from the comprehension and accurate prediction of near-wall processes.

Modern computational methods (direct numerical simulation, DNS; large eddy simulation, LES) aim at the description of temporally and spatially resolved turbulent flow fields and associated flow processes such as heat transfer and combustion. For DNS (depicting all turbulent scales), computational time dependence on pressure p , rotational speed n and stroke S scales with $p^3 n^3 S^6$ in ICE simulations (Frouzakis et al., 2017), leading to remarkable increases for large supercharged engines operated at high speeds. Although DNS will likely remain prohibitively expensive for engineering simulations in the near future (particularly if multi-cycle statistics are required), LES (resolving turbulent scales larger than a filtering threshold) has gained a firm standing as a complement to the widespread Reynolds-averaged (RANS) technique.

However, wall boundary layers pose a considerable challenge to LES (cf. Pope, 2004): for

21 accurate predictions of near-wall turbulence and heat transfer, near-wall grid resolution is
22 required to approach DNS standards. In ICEs, LES quality has been discussed by di Mare
23 et al. (2014) who present, among other metrics, the popular estimators based on modelled
24 turbulent kinetic energy and modelled viscosity. However, conventional near-wall metrics
25 such as scaled tangential resolution are less frequently studied. Considering the complex-
26 ity of ICE flows, it may not be straightforward to adopt near-wall criteria established for
27 flat-plate boundary layers (e.g. Choi and Moin, 2012). In fact, in-cylinder wall-resolved
28 LES investigations are scarce and unaffordable computational costs are associated with high
29 Reynolds numbers and complex engine configurations (Misdariis et al., 2015).

30 Wall-modelled LES (WMLES; referring here to wall stress models) and hybrid LES/RANS
31 methods (cf. (Larsson et al., 2016) for taxonomic perspectives) represent some of the pri-
32 mary avenues for alleviation of the near-wall issue (see reviews of Piomelli, 2008; Sagaut
33 et al., 2013; Larsson et al., 2016; Chaouat, 2017). Interest in such scale-resolving methods
34 has also been raised within the engine research community (Hasse, 2016). However, knowl-
35 edge of the functionality of different approaches is not extensive in the ICE context, where
36 wall modelling advances are not frequent and clear research gaps have been previously iden-
37 tified (Rutland, 2011). Many groups have applied models based on the law of the wall or
38 closely related correlations (e.g. Vermorel et al., 2009; Enaux et al., 2011; Misdariis et al.,
39 2015; Truffin et al., 2015; Schiffmann et al., 2016) while engine-targeted algebraic models
40 have also been adapted for WMLES (Plensgaard and Rutland, 2013). Conversely, some con-
41 temporary studies consciously disregard wall treatment (in favour of straightforward linear
42 gradient approximations), stating either modelling difficulty (Nguyen et al., 2016) or the
43 known departures from typical wall law (equilibrium) assumptions (He et al., 2017). In gen-
44 eral, near-wall flows or wall heat transfer are only rarely a focal component of ICE-related
45 LES papers.

46 In-cylinder flows differ considerably from channel or pipe flows, wherein the law of the
47 wall, for both wall shear stress and convective heat transfer, can often be considered to
48 be an acceptable approximation (White, 2006). As revealed by particle image velocimetry
49 (PIV) measurements (Jainski et al., 2013) and DNS (Schmitt et al., 2015a), scaled near-wall

50 velocity and temperature profiles in ICEs deviate from the law of the wall substantially. Such
51 variations are also influenced by engine operating conditions (Renaud et al., 2018) or local flow
52 regions dominated by (i) wall-parallel and (ii) stagnating contributions (Buhl et al., 2017b).
53 Renaud et al. (2018) found near-wall velocity profiles to resemble accelerated boundary layers
54 following impingement. Such an impinging flow type is well-known for local variation of scaled
55 profiles (Hattori and Nagano, 2004). ICE wall models should hence be applicable to many
56 types of flows in highly dynamic in-cylinder conditions. For RANS, improved wall models
57 accounting for considerable near-wall material property variations were introduced by Han
58 and Reitz (1997) and Angelberger et al. (1997). Later on, further advances have been made in
59 complex flows (e.g. Craft et al., 2002; Popovac and Hanjalic, 2007; Suga et al., 2013; Nuutinen
60 et al., 2014). Non-equilibrium models have recently been advocated in experimentally based
61 ICE near-wall layer investigations (Ma et al., 2017a,b) and have become a frequent topic in
62 recent WMLES studies not specifically pertaining to engines (Kawai and Larsson, 2013; Park
63 and Moin, 2014; Yang et al., 2015).

64 *1.2. Study objectives*

65 Based on the literature survey, there is a research gap in wall modelling for scale-resolving
66 ICE simulations. The recent DNS work on engine-like flows (Schmitt et al., 2014a,b, 2015a,b,
67 2016a,b; Schmitt and Boulouchos, 2016) provides a unique opportunity to benchmark various
68 approaches. Here, existing methods are assessed by implementing algebraic WMLES method-
69 ologies based on standard wall laws (WMLES-1) and engine-targeted models (WMLES-2).
70 In addition, an approach with a non-equilibrium wall model aimed at ICE flows (HLR-WT),
71 recently investigated in canonical flows (Keskinen et al., 2017), is further assessed here. Simu-
72 lations comprise three consecutive stages: (I) cold, multi-cycle reciprocating flow, (II) fuel-air
73 intake, and (III) charge compression, while stage III is the main focus of the present work.
74 The objectives of this study are stated as follows:

- 75 1. Comparing with the DNS data, assess the predictive ability of the approaches in terms
76 of mean quantities such as global wall heat transfer.
- 77 2. Examine how the specific near-wall profiles found in the DNS are reproduced with the

78 methods.

79 3. Analyse how focal physical near-wall mechanisms observed in the reference results are
80 replicated in the present simulations.

81 4. Investigate result sensitivity to grid variations both in the core flow and in the near-wall
82 region.

83 The paper is structured so that turbulence modelling and near-wall methodologies are
84 presented in Sec. 2, while the present engine-like test case setting and utilised computational
85 grids are reported in Sec. 2.7. Results in Sec. 3 convey a brief overview of stages I to III
86 followed by volume-averaged quantities in the compression stroke. Observations are then
87 gradually taken to a more detailed level, highlighting approach and grid-specific differences
88 not easily evidenced through averaged metrics. Finally, a discussion attempts to convey
89 relevant practical aspects to the investigation.

90 2. Methodology

91 2.1. Governing equations

92 The present simulations consist of three stages (I-III) explained in detail in Sec. 2.7.
93 While stage I is based on an incompressible formulation (see Keskinen et al., 2017), we
94 next explain the methodology used herein for the compressible intake (II) and compression
95 (III) processes. The simulations provide numerical solutions to the filtered compressible
96 mass, momentum, energy and species transport equations. Utilising density-weighted ($\tilde{\cdot}$)
97 and non-density-weighted ($\hat{\cdot}$) filtering notations, the governing equations read in Cartesian
98 coordinates with the Einstein notation:

$$\frac{\partial \hat{\rho}}{\partial t} + \frac{\partial(\hat{\rho}\tilde{u}_j)}{\partial x_j} = 0 \quad (1)$$

$$\frac{\partial(\hat{\rho}\tilde{u}_i)}{\partial t} + \frac{\partial(\hat{\rho}\tilde{u}_j\tilde{u}_i)}{\partial x_j} = -\frac{\partial \hat{p}}{\partial x_i} + \frac{\partial \hat{\tau}_{ij}}{\partial x_j} - \frac{\partial \tau_{ij}^r}{\partial x_j} \quad (2)$$

$$\frac{\partial(\hat{\rho}\tilde{h})}{\partial t} + \frac{\partial(\hat{\rho}\tilde{u}_j\tilde{h})}{\partial x_j} = \frac{\partial \hat{p}}{\partial t} - \frac{\partial}{\partial x_j} (\hat{q}_j + q_j^r) + \tilde{u}_j \frac{\partial \hat{p}}{\partial x_j} + (\hat{\tau}_{ij} + \tau_{ij}^r) \frac{\partial \tilde{u}_i}{\partial x_j} \quad (3)$$

$$\frac{\partial(\hat{\rho}\tilde{Y}_m)}{\partial t} + \frac{\partial(\hat{\rho}\tilde{u}_j\tilde{Y}_m)}{\partial x_j} = -\frac{\partial}{\partial x_j} (\hat{f}_{j,m} + f_{j,m}^r) \quad (4)$$

99 where $\hat{\rho}$, \tilde{u} , \hat{p} , \tilde{h} and \tilde{Y}_m refer to density, velocity, pressure, static enthalpy and species mass
100 fraction, respectively, whereas quantities $\hat{\tau}_{ij}$, \hat{q}_j and \hat{f}_j respectively correspond to the viscous
101 stress tensor, heat flux vector and species flux vector. Unresolved (residual) quantities are
102 modelled in the residual stress tensor τ_{ij}^r , residual heat flux vector q_j^r and residual species
103 flux vector $f_{j,m}^r$, expressed here with an eddy-viscosity model

$$\tau_{ij}^r = \hat{\rho} (\widetilde{u_j u_i} - \tilde{u}_j \tilde{u}_i) = -2\mu_{mod} \tilde{S}_{ij}^d + \frac{2}{3} \delta_{ij} \left(\mu_{mod} \frac{\partial \tilde{u}_k}{\partial x_k} + \rho k_{mod} \right) \quad (5)$$

$$q_j^r = \hat{\rho} (\widetilde{u_j h} - \tilde{u}_j \tilde{h}) = -\frac{\mu_{mod}}{\text{Pr}_{mod}} \frac{\partial \tilde{T}}{\partial x_j} \quad (6)$$

$$f_{j,m}^r = \hat{\rho} (\widetilde{u_j Y_m} - \tilde{u}_j \tilde{Y}_m) = -\frac{\mu_{mod}}{\text{Sc}_{mod}} \frac{\partial \tilde{Y}_m}{\partial x_j} \quad (7)$$

104 where μ_{mod} is modelled viscosity, \tilde{S}_{ij}^d is the traceless deviator of the resolved strain rate tensor
105 $\tilde{S}_{ij} = 0.5 (\partial \tilde{u}_i / \partial x_j + \partial \tilde{u}_j / \partial x_i)$, \tilde{T} is temperature, k_{mod} is modelled turbulent kinetic energy,
106 Pr_{mod} is the modelled Prandtl number and Sc_{mod} is the modelled Schmidt number. Gases in
107 this study are considered ideal.

108 2.2. LES model

109 For WMLES and the LES zone of hybrid LES/RANS simulations, modelled viscosity
110 μ_{mod} equals μ_{sgs} determined according to the σ -model by Nicoud et al. (2011):

$$\mu_{sgs} = \hat{\rho} (C_\sigma \Delta)^2 \frac{\sigma_3 (\sigma_1 - \sigma_2) (\sigma_2 - \sigma_3)}{\sigma_1^2} \quad (8)$$

111 where $C_\sigma = 1.35$ is a model constant, $\Delta = V_{cell}^{1/3}$ is the filter width where V_{cell} is cell volume,
112 and $\sigma_1 \geq \sigma_2 \geq \sigma_3 \geq 0$ are singular values of the resolved velocity gradient tensor $\partial \tilde{u}_i / \partial x_j$.
113 The σ -model is an explicit subgrid-scale (SGS) model without transport equations or dy-
114 namic filtering. SGS contributions vanish in many physically justified scenarios and cubic
115 asymptotic behaviour is satisfied near solid walls. The model has been extensively validated
116 and used in various previous studies with simple geometries (e.g. Toda et al., 2014; Rieth
117 et al., 2014). High model suitability for engine-like flows was noted in the recent investigation
118 of Buhl et al. (2017a). Here, SGS kinetic energy and dissipation rate are estimated in analogy

119 to a model proposed by Mason and Callen (1986) for the Smagorinsky model:

$$k_{sgs} = \nu_{sgs}^2 / (C_s^2 \Delta^2 C_\mu^{1/2}) \quad (9)$$

$$\varepsilon_{sgs} = \nu_{sgs}^3 / (C_s \Delta)^4 \quad (10)$$

120 where $\nu_{sgs} = \mu_{sgs} / \hat{\rho}$, $C_s = 0.165$ and $C_\mu = 0.09$. For Eqs. (6) and (7), the modelled Prandtl
 121 and Schmidt numbers $\text{Pr}_{mod} = \text{Sc}_{mod} = 0.9$. Justified deviations in Pr_{mod} were noted to have
 122 little influence on the results of this study, likely due to limited extent of modelled turbulence.

123 2.3. Reference wall models

124 Two engine research-relevant algebraic WMLES-models are considered in this work.
 125 WMLES-1 combines a linear-power law for wall shear stress (Werner and Wengle, 1991)
 126 with a linear-log law for wall heat flux:

$$u^+ = \begin{cases} y^+, & y^+ \leq 11.81 \\ A(y^+)^B, & y^+ > 11.81 \end{cases} \quad (11)$$

$$T^+ = \begin{cases} \text{Pr } y^+ & y^+ \leq 5 \\ \min(\text{Pr } y^+, \kappa^{-1} \ln [C_T y^+]) & y^+ > 5 \end{cases} \quad (12)$$

127 where $A = 8.3$, $B = 1/7$, $C_T = 2.96$ and u denotes the wall-relative tangential velocity. Vari-
 128 able scaling follows $y^+ = \rho_w u_\tau y / \mu_w$, $u^+ = (u_c - u_w) / u_\tau$, $T^+ = \rho_w u_\tau c_{p,w} (T_w - T_c) / q_w$ where
 129 $u_\tau = (\tau_w / \rho_w)^{1/2}$ and subscripts c and w denote cell and wall values, respectively. The Werner-
 130 Wengle model, applied by e.g. Schiffmann et al. (2016), is functionally very similar to the
 131 two-layer linear-log law for velocity. Schmitt et al. (2007) first applied the logarithmic part
 132 of Eq. (12) with a log-law for velocity in a burner WMLES, and their model has been used
 133 in several ICE WMLES studies (Vermorel et al., 2009; Enaux et al., 2011; Misdariis et al.,
 134 2015).

135 Plensgaard and Rutland (2013) developed a formulation entailing an improved Werner-
 136 Wengle model (including an SGS contribution) and a modified heat flux approach based on
 137 the engine-targeted model of Han and Reitz (1997) (herewith, WMLES-2). The model was

138 tested in duct flows and impinging jets in addition to reacting engine flows (Plensgaard,
 139 2013), and is implemented here as

$$\tau_w = \begin{cases} 2\mu_w u / \Delta y, & u \leq \frac{\nu_w}{2\Delta y} A^{2/(1-B)} \\ \rho_w \left[\frac{1-B}{2} A^{\frac{1+B}{1-B}} \left(\frac{\nu_w + \nu_{k,c}}{\Delta y} \right)^{1+B} + \frac{1+B}{A} \left(\frac{\nu_w + \nu_{k,c}}{\Delta y} \right)^B u \right]^{2/(1+B)}, & u > \frac{\nu_w}{2\Delta y} A^{2/(1-B)} \end{cases} \quad (13)$$

$$q_w = \begin{cases} \frac{\rho_w u_\tau c_{p,w} T_c \ln(T_c/T_w)}{c_{hw} [7.483 \arctan(0.0935y^+)]}, & y^+ \leq 40 \\ \frac{\rho_w u_\tau c_{p,w} T_c \ln(T_c/T_w)}{c_{hw} [2.1 \ln(y^+) + 2.5]}, & y^+ > 40 \end{cases} \quad (14)$$

140 where Δy is the near-wall cell height. Eq. (13) differs from the original Werner-Wengle
 141 law by introducing a modelled viscosity based on the near-wall modelled kinetic energy
 142 $\nu_{k,c} = c_{mw} V_{cell}^{0.33} k_{mod,c}$ where $c_{mw} = 0.01$. In contrast to the present method (Eq. 9), the
 143 original approach employs a one-equation SGS model in the determination of k_{mod} , while
 144 model parameters $c_{mw} = 0.01$ and $c_{hw} = 0.8$ were introduced based on square duct flow
 145 calibration studies (Plensgaard and Rutland, 2013).

146 2.4. HLR-WT approach

147 2.4.1. Hybrid LES/RANS model

148 The present zonal approach (HLR) follows the work of Jakirlić et al. (2010) and involves
 149 a fixed LES/RANS interface (see (Jakirlić et al., 2011) for a dynamic approach). The RANS
 150 zone employs a low-Reynolds $k - \varepsilon$ turbulence model based on the model of Lien et al. (1996)
 151 with pertinent modifications detailed in our previous study (Nuutinen et al., 2014). Con-
 152 tinuity of modelled viscosity across the nominal LES/RANS interface is implicitly imposed
 153 by setting k_{sgs} and ε_{sgs} (Eqs. (9)-(10)) in the first cell of the LES domain via source terms
 154 (cf. (Jakirlić et al., 2011) for a more detailed description). Interfaces in this study are placed
 155 manually to a scaled wall-normal distance of $y_1^+ \approx \mathcal{O}(100)$ in maximum gradient conditions,
 156 while intake jet regions were set in the LES zone. Variation of this scaled distance ensues
 157 due to the transient process. Various interface positions between $\mathcal{O}(50)$ - $\mathcal{O}(600)$ have been
 158 applied with zonal approaches (e.g. Piomelli et al., 2003; Temmerman et al., 2005; Jakirlić
 159 et al., 2011). Based on numerical tests in the present setup (not shown herein for brevity), re-

160 sults were not noted to be very sensitive to the exact position of the interface, corresponding
 161 with previous canonical flow observations (Keskinen et al., 2017).

162 In the HLR approach, Eqs. (1)-(4) incorporate an effective filter width (Jakirlić et al.,
 163 2011; Sagaut et al., 2013): in the RANS zone, the model mimics an SGS model whose
 164 length scale corresponds to the SGS width at the LES/RANS interface, approaching the
 165 scale $l_{RANS} = k^{3/2}/\varepsilon$ close to the wall (Jakirlić et al., 2011). As noted in our previous work
 166 (Keskinen et al., 2017), modelled contribution depends on the interface position and on the
 167 local flow state. Pure Reynolds-averaged simulation (devoid of any resolved turbulent fluc-
 168 tuations) should not be expected in RANS zones. Furthermore, very low modelled viscosity
 169 values were previously noted around near-wall stagnation flow regions. Hence, in the present
 170 work, modelled viscosity is limited in nominal RANS zones as $\mu_{mod} = \max(\mu_{sgs}, \mu_{RANS})$ for
 171 enhanced computational stability.

172 2.4.2. 1-D non-equilibrium wall model

173 The wall treatment developed by Nuutinen et al. (2014) in the RANS context is specifically
 174 designed for engine-like boundary layers and engine wall heat transfer. The present hybrid
 175 LES/RANS implementation was previously benchmarked in incompressible channel and im-
 176 pinging jet flows (Keskinen et al., 2017). Starting from main grid data at two wall-adjacent
 177 cell layers, the model solves simplified 1-D turbulent boundary layer equations (TBLEs) for
 178 momentum and enthalpy:

$$\frac{d}{dy} \left(\underbrace{[\mu + \mu_{mod}]}_{\mu_{eff}} \frac{du}{dy} \right) = \overbrace{I_m}^{const.} \Rightarrow \frac{du}{dy} = \frac{\overbrace{\tau_w + I_m y}^{\tau(y)}}{\mu_{eff}} \quad (15)$$

$$\frac{d}{dy} \left(\underbrace{c_p \left[\frac{\mu}{Pr} + \frac{\mu_{mod}}{Pr_{mod}} \right]}_{k_{T,eff}} \frac{dT}{dy} \right) = \overbrace{I_h}^{const.} \Rightarrow \frac{dT}{dy} = \frac{\overbrace{q_w + I_h y}^{q(y)}}{k_{T,eff}} \quad (16)$$

179 where k_T is thermal conductivity. Solution is carried out on an equidistant 1-D subgrid with
 180 spacing smaller than one dimensionless wall unit. The central assumption is that the several
 181 terms within momentum (I_m) and enthalpy (I_h) imbalances are not explicitly modelled but

182 their collated profiles are assumed to be independent of y based on observations regarding
 183 convection and pressure gradient in backward-facing step and impinging jet flows (Popovac
 184 and Hanjalic, 2007). This represents a highly simplified but physically consistent approach
 185 in comparison to modelling only some of the terms individually (Larsson et al., 2016). The
 186 unknown imbalance term values are formed within the iterative routine, while μ_{eff} and $k_{T,eff}$
 187 profiles are determined using algebraic simplifications of a linear low-Reynolds $k - \varepsilon$ model
 188 (Lien et al., 1996). Temperature-dependent material property variations throughout the
 189 subgrid are concisely included in nondimensionalised equations via power law expressions.
 190 As a result from converged near-wall profiles, the routine provides wall shear stress and wall
 191 heat flux linearisation coefficients as well as modelled turbulence source terms for the main
 192 solver. Appendix A provides further details regarding the model.

193 *2.5. Wall model discussion*

194 The common objective of the investigated approaches is to provide accurate wall flux
 195 predictions based on information that can be gathered from different components of the
 196 main grid solution. Table 1 displays a summary of wall model characteristics such as in-
 197 put and output quantities. Although the 1-D model formulation is much more complicated
 198 in comparison to the algebraic models, it is worth recalling that the latter can be consid-
 199 ered to represent simplified solution sets for TBLEs where non-equilibrium terms cancel out
 200 ($I_m = I_h = 0$). Furthermore, equilibrium models may not be as restrictive as their formu-
 201 lation suggests due to the non-equilibrium effects inherently captured by LES in the outer
 202 layer (Larsson et al., 2016). For ICE boundary layers, the straightforward incorporation
 203 of material property variations should be considered an advantage of both equilibrium and
 204 non-equilibrium 1-D models.

205 An additional difference between the approaches arises from the sequence in which the
 206 output quantities are evaluated. In WMLES-1 and WMLES-2, τ_w is first determined while
 207 the result (u_τ) is fed to the convective heat transfer model, cf. Eqs. (12) and (14). Hence, an
 208 explicit link between τ_w and q_w is constructed in line with the Reynolds analogy, whereof some
 209 effects will be discussed in Sec. 3.6. In HLR-WT, Eqs. (15)-(16) are iterated simultaneously
 210 while the output quantities are linked only implicitly through material property and modelled

Table 1: Characteristic description of the present wall-modelled approaches. In addition to the listed near-wall (NW) grid point data, all models employ material properties, wall velocity and wall temperature as input.

	WMLES-1	WMLES-2	HLR-WT
Wall model format	algebraic	algebraic	simplified 1-D TBLE
Solution method	explicit	explicit	iterative
Input data (τ_w)	u	u, μ_{mod}	$u, T, \mu_{mod}, k_{mod}, \varepsilon_{mod}$
Input data (q_w)	T, u_τ	T, u_τ	
Input data location	first NW grid point	first NW grid point	first and second NW grid points
Modelled non-equilibrium	-	-	constant imbalance model
Material property variation	-	embedded (μ, ρ)	μ, c_p, k_T, ρ
Output data	τ_w, q_w	τ_w, q_w	τ_w, q_w , source terms for $k_{mod}, \varepsilon_{mod}$

211 viscosity profiles.

212 2.6. Numerical aspects

213 Simulations are carried out with the Star-CD v. 4.20 software (licensed by CD-Adapco).
 214 The momentum equation is discretised with central differencing whereas for scalar quanti-
 215 ties, including modelled turbulence equations, the monotone advection reconstruction scheme
 216 (MARS) is employed (CD-Adapco, 2013). The pressure-implicit splitting of operators (PISO)
 217 method is utilised for pressure-velocity coupling. Grid resolutions are discussed in stage-
 218 specific subsections. The SGS model, hybrid LES/RANS interfacing and wall models of the
 219 present work are implemented as user subroutines.

220 2.7. Test cases

221 Figure 1 shows a general schematic of the case, originating from the experimental flow
 222 study of Morse et al. (1979) and further expanded by DNS investigations (Schmitt et al.,
 223 2014a,b, 2015a,b, 2016a; Schmitt and Boulouchos, 2016). Here, we divide the present com-
 224 putational tasks into three stages, consistent with the manner in which the DNS results
 225 were generated. Preliminary stages I and II aim to (1) benchmark the methodology in a
 226 cold engine-like flow, and to (2) generate several bottom dead centre (BDC) conditions for
 227 compression stroke simulations, thus permitting the assessment of cycle selection influence.

228 2.7.1. Stage I: Multiple cold flow cycles

229 Consecutive cycles of a valve-piston assembly are simulated with a compression ratio
 230 of 3:1, containing air at atmospheric conditions, corresponding to the original experiment

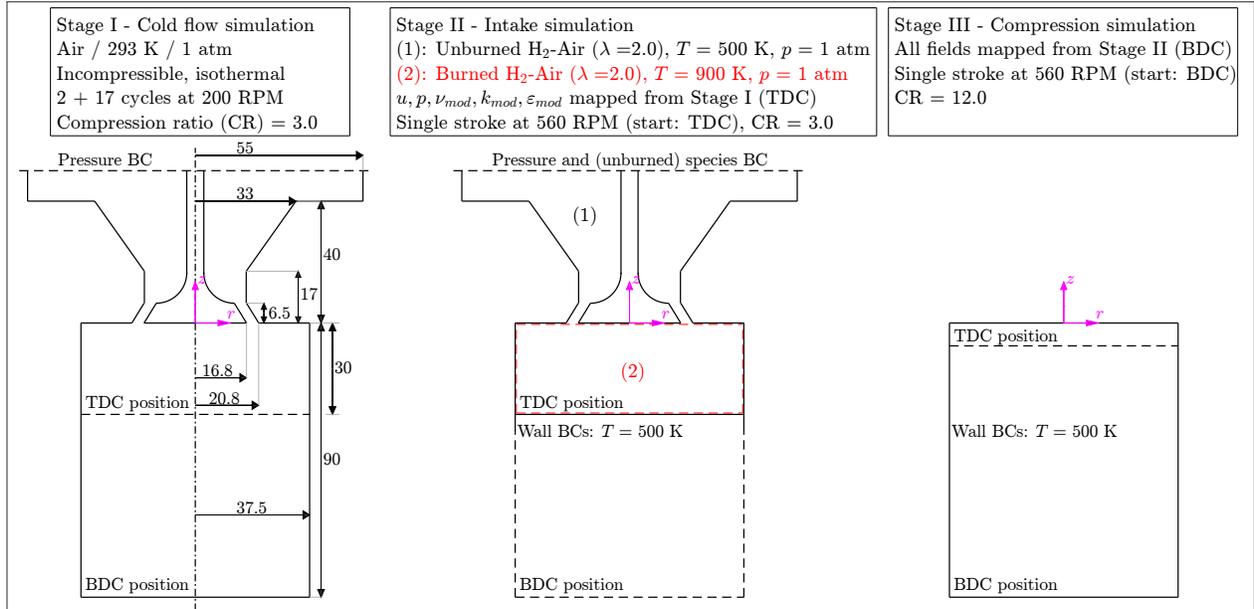


Figure 1: Schematic description of the three simulation types in the present study: consecutive cold flow cycles (stage I), single intake cycle (II) and single compression cycle (III). System dimensions are expressed in millimetres.

231 (Morse et al., 1979) as well as several computations (e.g. Schmitt et al., 2014b; Keskinen
 232 et al., 2015; Montorfano et al., 2015; Buhl et al., 2017a). In contrast to actual engine crank
 233 kinematics, piston movement is prescribed by simple sinusoidal motion at a rotational speed
 234 of 200 revolutions per minute (RPM). The filtered result quantities are averaged spatially in
 235 the azimuthal direction and phase-averaged over the simulated cycles. The DNS and LES
 236 studies cited above simulated 6 to 13 consecutive cycles, while the present work includes 17
 237 cycles (in addition to the first two cycles which are disregarded). Stage I and II computations
 238 are carried out with a grid containing 2.3×10^6 hexahedral/polyhedral cells at BDC and
 239 1.1×10^6 at top dead centre (TDC). This grid count clearly exceeds early LES studies of the
 240 case (e.g. Haworth and Jansen, 2000, $N = 0.15 \times 10^6$) but is also lower than contemporary
 241 LES investigations (Montorfano et al., 2015; Keskinen et al., 2015; Buhl et al., 2017a, $N =$
 242 4.6×10^6 , $N = 5.1 \times 10^6$, $N = 14.5 \times 10^6$, respectively).

243 2.7.2. Stage II: Intake stroke

244 The flow field at the end of the preceding cycle was noted by Schmitt et al. (2014a) as
 245 an influential factor in the dominant processes of jet development and vortex ring genera-
 246 tion. In stage II, an intake stroke is initialised from TDC, maintaining the velocity, pressure

Table 2: Dimensional metrics for stage III compression stroke simulations. Wall-normal (y_1) tangential (Δ_{tan} , see Fig. 2), axial (Δ_z) and azimuthal ($R_c\Delta\phi$) spacings are provided here.

	M1	M1-CW	M2	M2-CW	M3
Cells (BDC)	0.44×10^6	0.43×10^6	2.6×10^6	2.4×10^6	6.4×10^6
Cells (TDC)	0.65×10^5	0.65×10^5	0.31×10^6	0.24×10^6	0.69×10^6
y_1 (mm)	0.14	0.20	0.12	0.20	0.12
Δ_{tan} (mm)	1.2	1.2	0.59	0.59	0.44
Δ_z (mm)	1.0	1.0	0.60	0.60	0.40
$R_c\Delta\phi$ (mm)	1.4	1.4	0.70	0.70	0.53

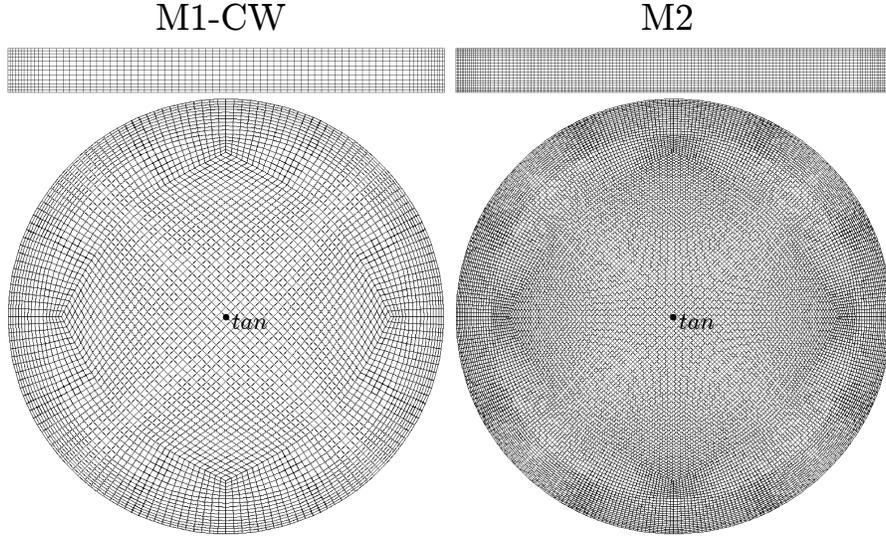


Figure 2: Vertical (top; TDC piston position) and horizontal (bottom) cutouts of grids used in stage III computations. Coarse & coarse-wall (M1-CW; left) and intermediate & nominal-wall (M2; right) variants are shown here. Annotated points in the grid images indicate the measurement location for Δ_{tan} in Table 2 and Fig. 3.

247 and modelled turbulence fields from a selected stage I cycle. A nominal cycle (A) and two
248 differing cycles (B & C) are determined based on azimuthally averaged flow fields (see Ap-
249 pendix B). The following additional considerations reflect the DNS reference (Schmitt et al.,
250 2015a): homogeneous mixtures of burned (in-cylinder) and unburned (intake) gases, based
251 on equilibrium chemistry, are initialised with respective temperatures of 900 K and 500 K.
252 Hydrogen (H_2) is employed as the fuel with a relative air-fuel ratio (λ) of 2.0 compared to
253 stoichiometry. A fixed wall temperature condition of $T_w = 500$ K is set at the walls and the
254 engine speed is set at 560 RPM.

255 *2.7.3. Stage III: Compression stroke*

256 Stage III is initialised from the BDC result of stage II, while the geometric compression
257 ratio is increased from 3:1 to 12:1 in analogy to the DNS. Three core flow (off-wall) resolutions
258 (M1, M2, M3) and two near-wall resolutions (nominal, coarse-wall [CW]) are considered in
259 order to assess the influence of both grid variation types independently. Table 2 provides
260 basic dimensional metrics for the different grids (shown in Fig. 2), while Fig. 3 illustrates
261 how the highly dynamic compression stroke influences dimensionless metrics. The first wall-
262 normal grid points are set to locations that eventually exceed the viscous sublayer and are
263 thus interesting from the wall modelling perspective. The locations are also within the
264 boundary layer thickness: in Fig. 3, $\delta_{90,t}$ represents the wall-normal distance at which the
265 mean temperature gradient has decreased by 90% in comparison to its maximum value. This
266 differs from the classical definition due to the time-dependent mean flow outside the boundary
267 layer (Schmitt et al., 2015a). The reference DNS grid initialises at 90×10^6 nodes and is
268 refined at 306°CA after top dead centre (ATDC) to 135×10^6 nodes (Schmitt et al., 2015a).
269 The present computations are carried out without intermittent refinement while cell layer
270 removal is employed to maintain a near-constant axial resolution.

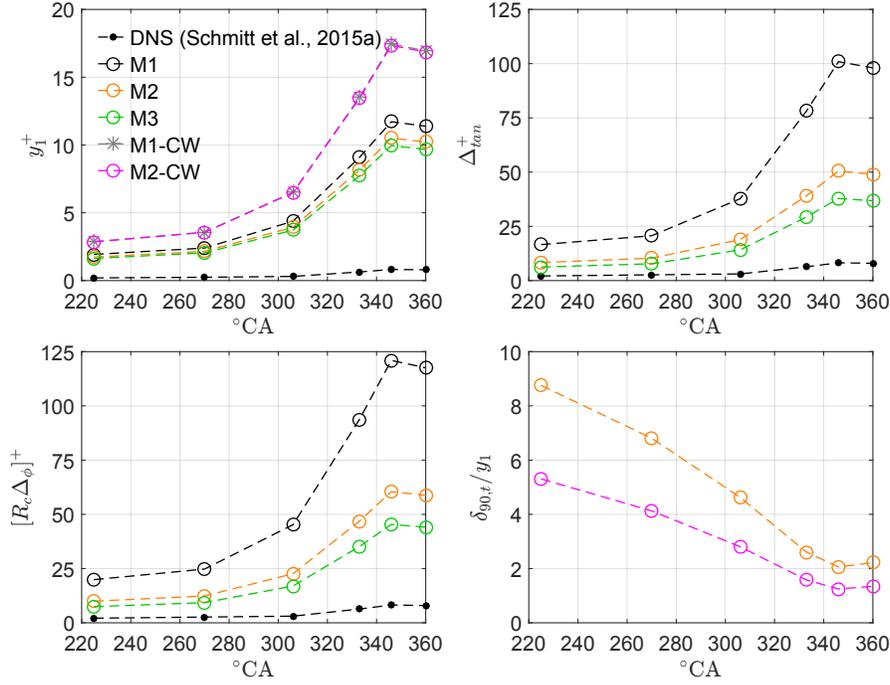


Figure 3: Variation of near-wall grid metrics throughout the compression stroke. Dimensionless wall-normal spacing (top left), tangential spacing (at the centre of the cylinder head; top right), azimuthal spacing at the cylinder liner (bottom left), and scaled thermal boundary layer thickness (bottom right). Scaling has been carried out according to cylinder head-averaged shear velocity and thermal boundary layer thickness observations in the reference DNS.

271 3. Results

272 The initial conditions for stages II and III are generated from stage I based on the HLR-
 273 WT model. Next, we show that the data in stage I is generated consistently with the
 274 model. For brevity, in Secs. 3.1-3.3 we only show results for HLR-WT, while model-to-
 275 model comparison is carried out for the compression stroke starting from Sec. 3.4.

276 3.1. Stage I (HLR-WT)

277 Fig. 4 displays instantaneous velocity and modelled viscosity fields, elucidating the char-
 278 acteristics of the cyclic process during intake. Coherent flow features such as jet orientation
 279 (a), toroidal vortex ring location and intensity (b) as well as the advance of wall jets (c) are
 280 seen to vary between cycles. Concurrently, modelled viscosity frames, split into two halves,
 281 show the local influence of turbulence modelling. The left-hand side shows the modelled
 282 viscosity (ν_{mod}) whereas the right-hand side displays the additive influence of the near-wall
 283 hybrid model ($\nu_{mod} - \nu_{sgs}$). Unlike the velocity field images, the two viscosity image halves
 284 are mirrored for a clearer comparison: both sides display fields corresponding to the left-

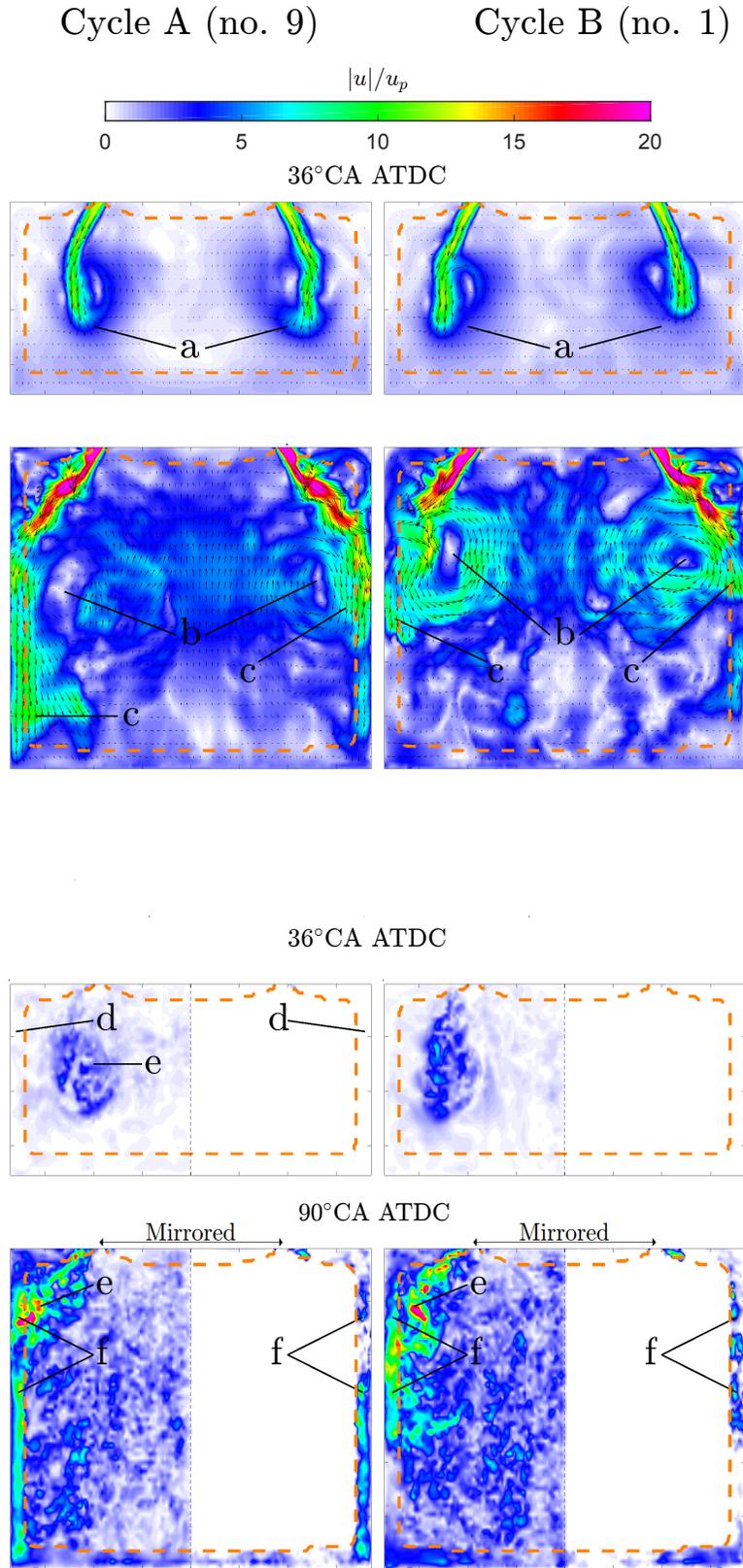


Figure 4: Stage I: velocity magnitude (top, scaled with mean piston velocity u_p) and modelled viscosity (bottom, scaled with molecular viscosity) snapshots on cycle A and cycle B along the same $r - z$ sampling plane. The orange dashed line denotes the LES/RANS interface position. Differences in dominant flow features including free jet orientation (a), vortex ring formation (b) and wall jet formation (c) are noted. On the LES side of the interface, modelled viscosity is entirely due to the SGS model (e). The zonal hybrid model is largely inactive during low Re conditions (d), activating with changing near-wall flow conditions (f).

285 hand side of the velocity fields. Due to the transient nature of the process, the flow Reynolds
 286 number and modelled contribution fluctuate considerably. During early intake (36°CA), ν_{mod}
 287 arises almost exclusively from the SGS model (**e**), while the hybrid model is suppressed due
 288 to low modelled production and interface SGS quantities (**d**). In such conditions, the wall
 289 model employs SGS quantities as input. Later (90°CA), higher modelled turbulence contri-
 290 bution can be noted at intake jets (**e**) and wall jets (**f**). (**e**) is again due to the SGS model
 291 while hybrid model activation is noted in the near-wall zones (**f**).

292 Fig. 5 illustrates phase and azimuth-averaged ($\langle \cdot \rangle$) mean axial velocities from the present
 293 HLR-WT simulation, compared with DNS (Schmitt et al., 2014b, $N = 57.8 \times 10^6$; spectral
 294 element code Nek5000) and LES (Keskinen et al., 2015, $N = 5.1 \times 10^6$; finite volume code
 295 OpenFOAM). Unlike the present work, cell layer removal and addition were not incorporated
 296 in the DNS and LES. The mean velocity profiles in Fig. 5 show a fair correspondence between
 297 all cases. While the HLR-WT shows a slight deviation in the initial jet orientation at 90°CA ,
 298 the wall jet velocity profile is better described with the present computations compared to
 299 the reference LES. In general, deviations with the DNS result decrease when timing advances
 300 to 144° ATDC.

301 Axial velocity fluctuations (Fig. 6) also display good correspondence, although some
 302 overprediction is noted in near-wall values. When comparing fluctuation results it should be
 303 recalled that the reference LES result does not report a modelled fraction. The SGS model
 304 comparison of Buhl et al. (2017a) indicated that various models can provide a good agreement
 305 with experimental and DNS references. HLR-WT with the Smagorinsky model (not shown
 306 here) results in a relatively similar correspondence as the σ -model. Overall, the present mean
 307 and fluctuating velocity profiles provide a match to DNS which is at least equivalent to the
 308 reference LES which employs a different code and a finer grid.

309 3.2. Stage II (HLR-WT)

310 Fig. 7 displays azimuthally averaged ($\langle \cdot \rangle_\phi$) temperature and velocity fields at the end of
 311 the intake stroke. The flow field is dominated by the toroidal vortex ring as a result of the
 312 incoming annular jet of fresh fuel-air mixture. In addition to the substantial local variations
 313 and asymmetry expected from scale-resolving simulations (not shown here), averaged quan-

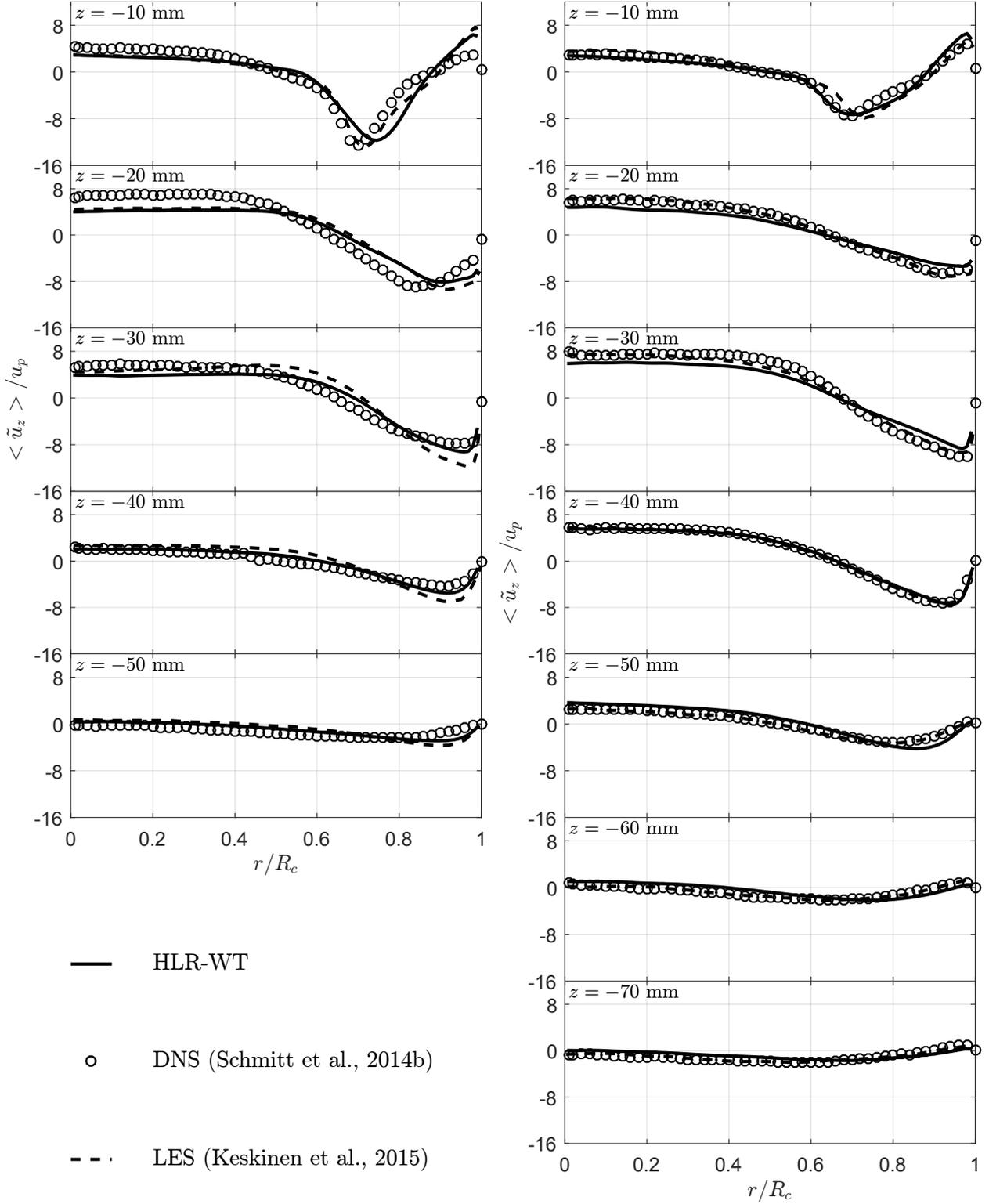


Figure 5: Stage I: axial mean velocities at observation planes, 90°CA ATDC (left) and 144°CA ATDC (right). Present results are averaged spatially in the azimuthal direction and phase-averaged over 17 consecutive cycles. Radial position r is scaled with the cylinder radius R_c .

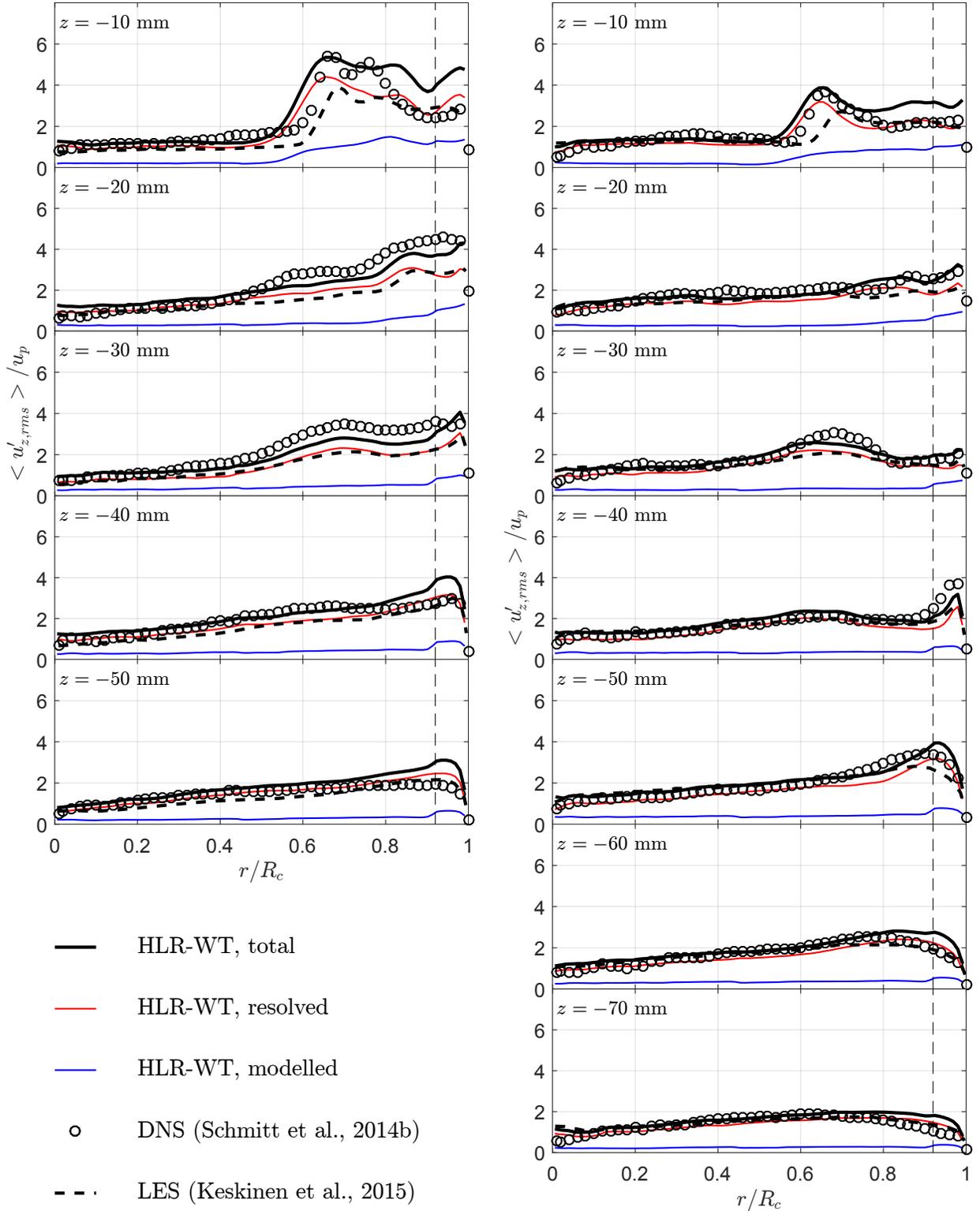


Figure 6: Stage I: axial rms velocity fluctuations at observation planes, 90°CA ATDC (left) and 144°CA ATDC (right). For the present HLR-WT cases, both resolved and modelled fractions are shown, while the vertical dashed lines denote the LES/RANS interface. Present results are averaged spatially in the azimuthal direction and phase-averaged over 17 consecutive cycles.

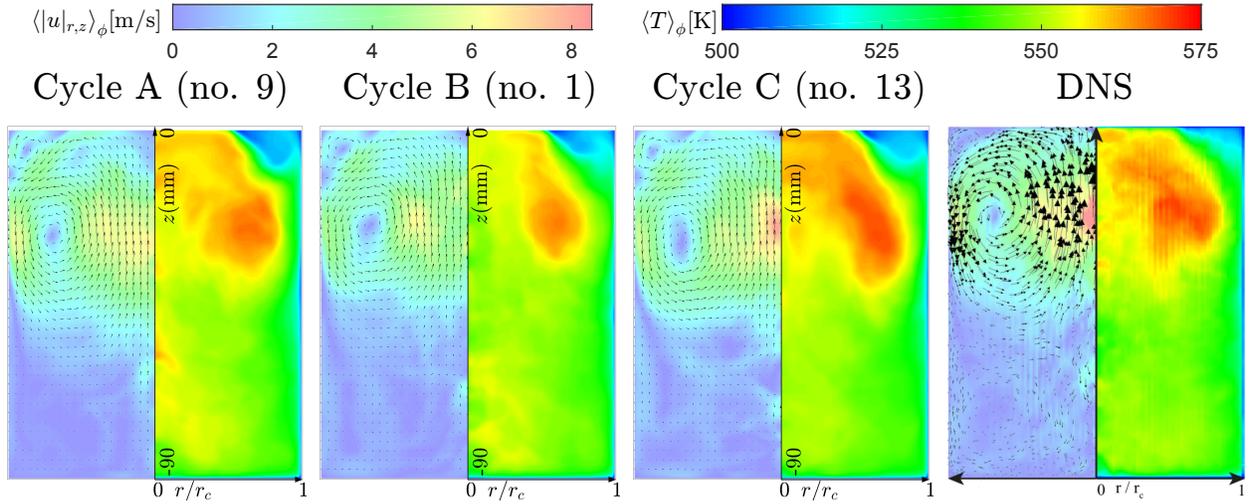


Figure 7: Stage II with different initialisation cycles (A, B, C): azimuthally averaged $r - z$ -velocity fields (left half-frames) and azimuthally averaged temperature fields (right half-frames) at BDC. HLR-WT (three leftmost frames) and the reference DNS (Schmitt et al., 2015a, right).

314 tity fields vary depending on the initial fields imported from stage I computations. Foremost
 315 differences are observed in vortex ring and thermal field positioning. Despite slight variation
 316 between each cycle (A, B, C) and the reference DNS, the nominal cycle (A) BDC conditions
 317 appear to pose a sensible starting point for stage III.

318 3.3. Stage III overview (HLR-WT)

319 For brevity, an overview of simulation characteristics is shown here only for the HLR-WT
 320 model, whereas Secs. 3.4-3.7 concentrate on model-to-model assessment. Qualitatively sim-
 321 ilar results are however obtained also for the other approaches. The temperature and fuel
 322 mass fraction fields in Fig. 8 visualise how mixture formation progresses during the compres-
 323 sion stroke. Close to BDC at 225°C_A, temperature variation is $\mathcal{O}(100 \text{ K})$ while the fuel-air
 324 mixture is still relatively inhomogeneous. Corresponding with initial unburned/burned con-
 325 ditions of stage II, thermal and fuel mass fraction fluctuations are negatively correlated.
 326 Conversely, at TDC, fuel and air are relatively well-mixed ($\overline{Y(H_2)'}_{rms,V} / \overline{Y(H_2)}_V = \mathcal{O}(10^{-3})$,
 327 where $\overline{\cdot}_V$ denotes volume-averaging) whereas differences have increased in the thermal field
 328 ($\overline{T'}_{rms,V} / \overline{T}_V = \mathcal{O}(10^{-1})$) due to concurrent compression and wall heat transfer.

329 While the LES/RANS interface in Fig. 8 places a considerable portion of the charge
 330 in the RANS zone, only minor and very localised influence thereof (where $\nu_{mod} > \nu_{sgs}$) is
 331 observed. Hence, the stage III HLR-WT computations are close to the WMLES simulations

360°CA ATDC

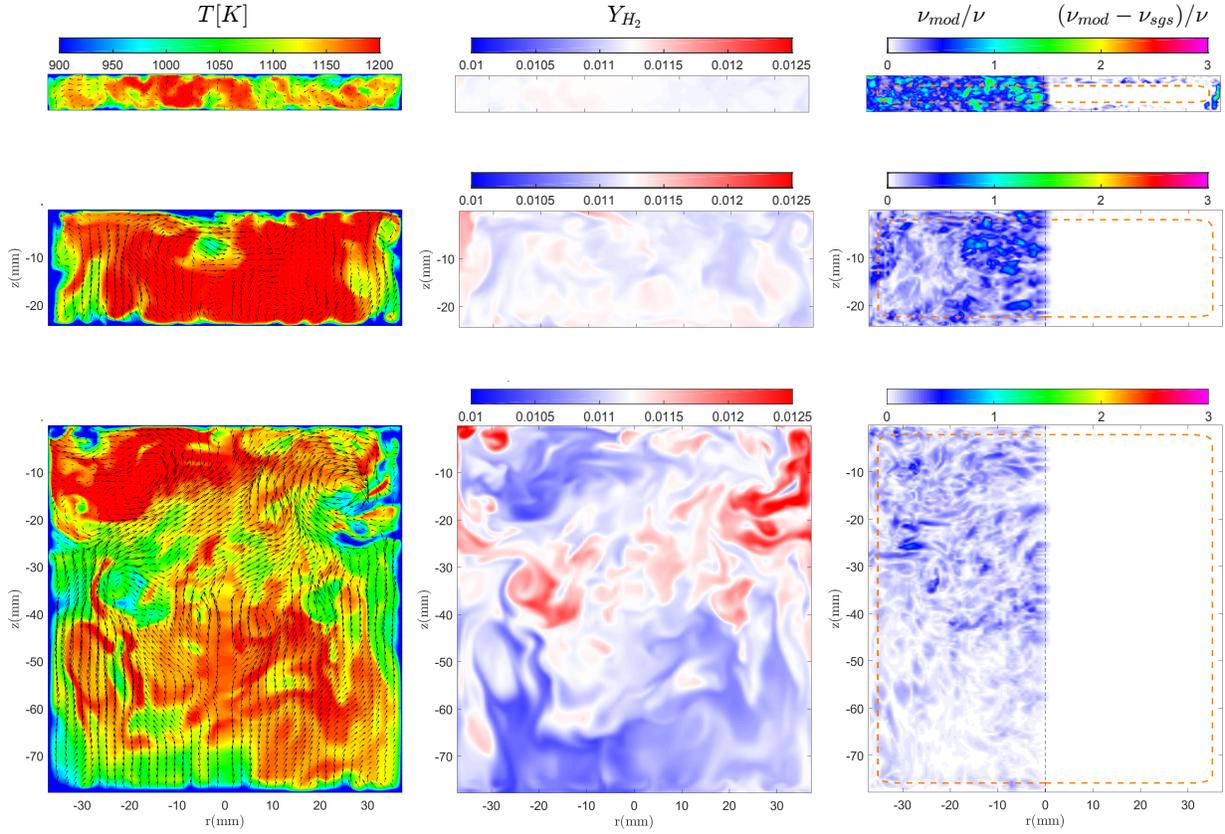


Figure 8: Stage III: instantaneous temperature (left, overlaid with $r - z$ velocity vectors), H_2 mass fraction (centre) and modelled viscosity (right) field snapshots throughout the compression stroke with HLR-WT (M3). The modelled viscosity snapshots show the LES/RANS interface (denoted by orange dashed lines) and are divided into halves showing ν_{mod} and $(\nu_{mod} - \nu_{sgs})$.

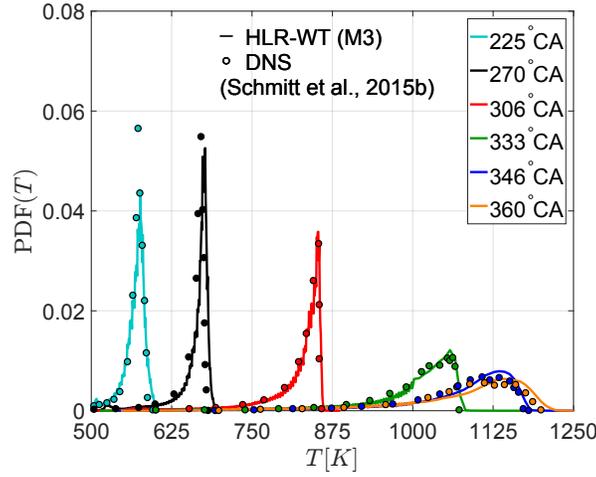


Figure 9: Stage III: Temperature PDFs at different time instances with the HLR-WT method (M3 grid) compared with the DNS reference (Schmitt et al., 2015b).

332 in terms of modelled contribution. Large thermal near-wall fluctuations convecting into the
 333 core charge are noted, corresponding with observations in the DNS (Schmitt et al., 2016a)
 334 and experimental investigations (Kaiser et al., 2013). Fig. 9 shows temperature probability
 335 density functions (PDFs) of the charge at different time instances. The influence of wall heat
 336 transfer towards TDC is evidenced by increasingly broader and shallower distributions.

337 3.4. Volume-averaged metrics

338 Table 3 reports volume-averaged results at the middle of the compression stroke (270°CA)
 339 and at TDC (360°CA) for all the studied approaches and grids. The most significant
 340 approach-specific differences arise in the TDC thermal metrics, visualised in Fig. 10. WMLES-
 341 1-based computations result in the highest mean temperature deviations, and thermal fluc-
 342 tuation levels are considerably lower than in the WMLES-2 and HLR-WT cases. Increased
 343 resolution generally appears to improve results. In Table 3, the total fluctuation energy \bar{k}_V
 344 and mean flow kinetic energy \overline{KE}_V are defined as

$$\bar{k}_V = 0.5 \left[\overline{(\tilde{u}_r - \langle \tilde{u}_r \rangle_\phi)^2 + (\tilde{u}_\phi - \langle \tilde{u}_\phi \rangle_\phi)^2 + (\tilde{u}_z - \langle \tilde{u}_z \rangle_\phi)^2} \right]_V + \overline{k_{modV}} \quad (17)$$

$$\overline{KE}_V = 0.5 \left(\overline{\langle \tilde{u}_r \rangle_\phi^2 + \langle \tilde{u}_\phi \rangle_\phi^2 + \langle \tilde{u}_z \rangle_\phi^2} \right)_V \quad (18)$$

345 where k_{mod} refers to either k_{RANS} or k_{sgs} . A relative decline of turbulent fluctuations is noted
 346 when approaching TDC, in correspondence with the study of Mandanis et al. (2017). A late

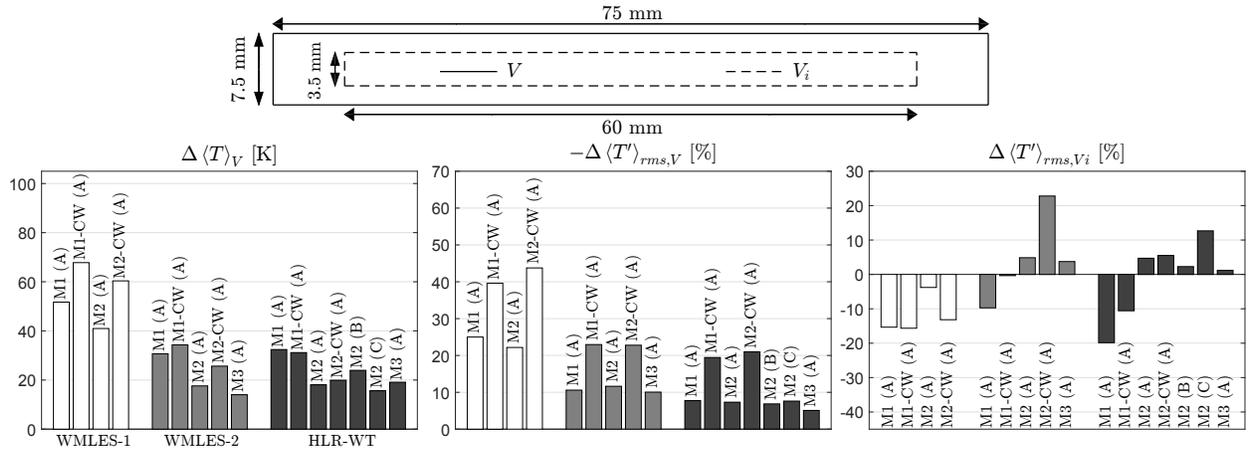


Figure 10: Stage III: visualisation of thermal metric differences between wall modelling approaches and DNS at TDC according to methodology, grid and cycle. Top: schematic of the cylinder geometry at TDC, showing the volume (V) and the inner volume (V_i). Volume-averaged mean temperature (left), volume-averaged temperature rms fluctuation (centre), inner volume-averaged temperature rms fluctuation (right).

347 compression decrease in fluctuating content with respect to experiments (Borée et al., 2002)
 348 was also noted by Toledo et al. (2007) in a simplified model engine. In the present low-order
 349 framework with non-uniform grids, numerical dissipation should be expected to have some
 350 effect as observed by Le Ribault et al. (2006) in the compression of a Taylor vortex. Noting
 351 the comparable sensitivity between (i) the improved approaches (WMLES-2 & HLR-WT),
 352 (ii) grid resolution, and (iii) the different initialisation cycles (A, B, C) in the results of Fig.
 353 10 and Table 3, it appears challenging to make a systematic statement on the differences
 354 between WMLES-2 and HLR-WT. However, the improvements on WMLES-1 in terms of
 355 volume-averaged temperature and thermal fluctuations represent a distinct outcome of the
 356 presented results.

357 To explain the differing results at TDC, Fig. 11 depicts the temporal evolution of total
 358 heat transfer rate through cylinder walls. Minor differences to actual engine processes should
 359 be expected herein due to the sinusoidal piston positioning. Up to mid-compression, where
 360 grid resolution requirements remain lenient (Fig. 3) and wall modelling has little impact, only
 361 minor variation is noted between the cases. Thereafter, heat transfer rates increase markedly
 362 and WMLES-1 in particular begins to deviate from the DNS reference, especially with the
 363 CW grids. Accuracy is considerably improved with the WMLES-2 and HLR-WT approaches,
 364 whose total heat transfer trends are very similar with the latter displaying slightly lower grid
 365 sensitivity. Again, initialisation cycle selection has a noticeable but relatively mild effect on

Table 3: Collated results from stage III computations at two instances (270, 360°CA) of the compression stroke. In contrast to volume averaging (subscript V), Vi denotes an internal part of the cylinder, limited by a 30 mm radius as well as (1) 7.5 mm (piston top/cylinder head) wall vicinity (up to 270°CA), (2) 2 mm wall vicinity (after 270°CA). For thermal metrics at 360°CA, the five most (*) and least (†) accurate correspondences to the DNS are highlighted.

Approach	Grid	Cycle	270°CA					360°CA				
			\bar{T}_V [K]	$\bar{T}'_{rms,V}$ [K]	$\bar{T}'_{rms,Vi}$ [K]	\bar{k}_V [m ² /s ²]	\overline{KE}_V [m ² /s ²]	\bar{T}_V [K]	$\bar{T}'_{rms,V}$ [K]	$\bar{T}'_{rms,Vi}$ [K]	\bar{k}_V [m ² /s ²]	\overline{KE}_V [m ² /s ²]
<i>DNS</i>			<i>659</i>	<i>29.7</i>	<i>6.8</i>	<i>2.50</i>	<i>1.30</i>	<i>1053</i>	<i>119.9</i>	<i>47.3</i>	<i>0.98</i>	<i>0.11</i>
WMLES-1	M1	A	661	29.1	6.0	1.84	1.23	1105†	89.9†	40.0†	0.57	0.04
WMLES-1	M1-CW	A	661	28.2	6.4	1.87	1.21	1121†	72.4†	39.9†	0.55	0.04
WMLES-1	M2	A	660	29.1	6.1	1.89	1.25	1094†	93.3	45.5*	0.54	0.08
WMLES-1	M2-CW	A	660	27.9	6.4	1.90	1.25	1113†	67.4†	41.1†	0.63	0.07
WMLES-2	M1	A	661	29.2	6.0	1.84	1.23	1084	107.2	42.7	0.58	0.04
WMLES-2	M1-CW	A	661	28.5	6.4	1.88	1.21	1087†	92.4†	47.1*	0.57	0.04
WMLES-2	M2	A	660	29.2	6.1	1.88	1.25	1071*	105.9	49.6	0.55	0.07
WMLES-2	M2-CW	A	660	28.2	6.1	1.90	1.25	1079	92.6†	58.1	0.59	0.06
WMLES-2	M3	A	660	29.7	7.1	1.95	1.24	1067*	107.8	49.1*	0.59	0.04
HLR-WT	M1	A	661	29.3	6.0	1.85	1.23	1086	110.6*	37.9†	0.55	0.04
HLR-WT	M1-CW	A	661	29.0	6.1	1.86	1.21	1084	96.6	42.3	0.52	0.06
HLR-WT	M2	A	660	29.4	6.2	1.89	1.26	1071*	111.1*	49.5	0.52	0.08
HLR-WT	M2-CW	A	660	28.8	6.3	1.90	1.25	1073	94.7	49.9	0.54	0.05
HLR-WT	M2	B	659	29.3	6.0	1.61	1.24	1077	111.7*	48.4*	0.50	0.05
HLR-WT	M2	C	660	29.2	6.4	1.33	1.53	1069*	110.8*	53.3†	0.55	0.10
HLR-WT	M3	A	661	29.8	7.1	1.95	1.25	1072*	113.8*	47.9*	0.56	0.06

366 the trends.

367 3.5. Near-wall profiles

368 The wall-bounded flows in ICEs are highly non-standard in terms of their structure and
369 the commonly utilised scaling laws. Hence, nondimensional velocity and temperature profiles
370 provide an informative impression of wall model functionality. In Fig. 12, such profiles
371 are plotted at 270°CA, 306°CA and 346°CA for the M1-CW and M2 grids. Velocity is
372 scaled here as $|u|^+ = |u|/\bar{u}_{\tau 90}$, wall-normal distance as $z^+ = (z/\nu_w)\bar{u}_{\tau 90}$, and temperature as
373 $T^+ = (T_w - T)\rho_w c_{p,w}\bar{u}_{\tau 90}/\bar{q}_{w 90}$. $\bar{\cdot}_{90}$ denotes instantaneous spatial averaging over 0-90 % of
374 the cylinder radius in analogy with the DNS.

375 Several contrasting properties can be highlighted between the models. Both WMLES-1
376 and WMLES-2 yield velocity scaling closer to the Werner-Wengle power law (Eq. 11) and
377 the linear-log law than to the DNS results (a). Hence, excessive $|u|^+$ values (representing
378 underprediction of u_τ) are observed towards TDC. The finer near-wall grid supplies better
379 results as the near-wall grid point is located within the viscous sublayer for a longer time,
380 which is an expected result based on the observations of Ma et al. (2017a). Scaled tem-

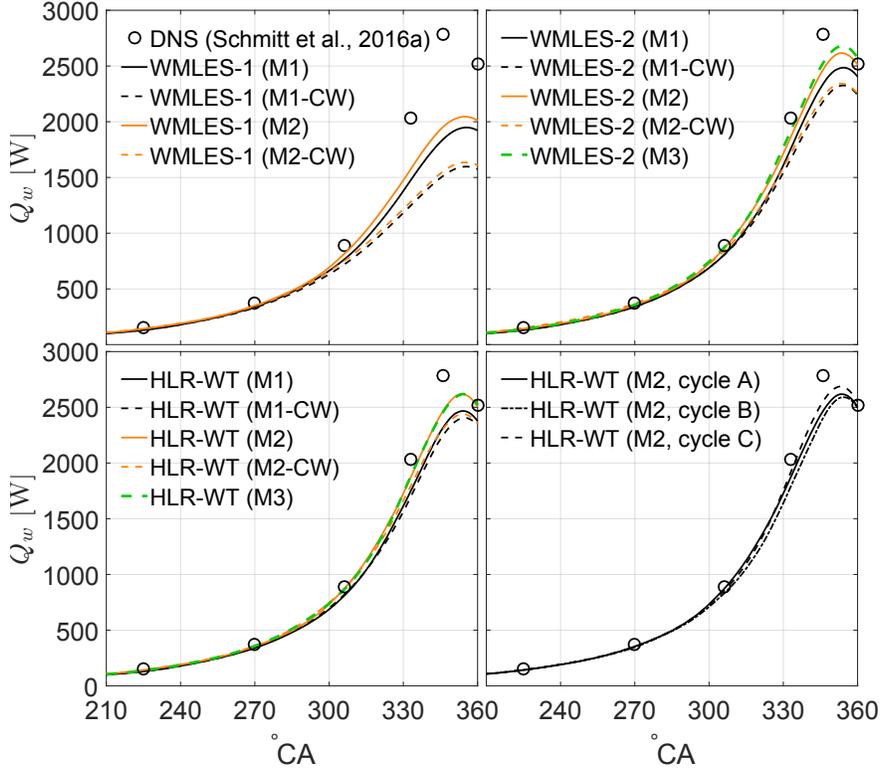


Figure 11: Stage III: total wall heat transfer rate throughout the compression stroke with WMLES-1 (top left), WMLES-2 (top right) and HLR-WT (bottom left) approaches and different grids with cycle A. The influence of initialisation cycle selection is shown with HLR-WT and the M2 grid (bottom right).

381 perature profiles however differ conspicuously between WMLES-1 and WMLES-2, with the
 382 former erroneously following a linear-logarithmic trend (b), consistent with its formulation.
 383 Remarkably, WMLES-2 results in relatively accurate thermal scaling despite the inclusion of
 384 the mismatched u_τ as an input to the heat transfer model.

385 In contrast to the two algebraic models, HLR-WT scaling appears relatively accurate and
 386 consistent between velocity and thermal boundary layers, indicating that fairly appropriate
 387 predictions are obtained for both wall shear stress and wall heat flux over the highly dy-
 388 namic compression stroke. Furthermore, this mean profile result is replicated with different
 389 grids in terms of both near-wall and core flow resolution. Such results could potentially be
 390 expected from 1-D non-equilibrium models: Ma et al. (2017b) reported favourable results for
 391 both momentum and thermal boundary layers in their measurement-based near-wall model
 392 comparison. In comparison to their work (Ma et al., 2017a,b), the present non-equilibrium
 393 model is conceptually simpler as individual imbalance contributions are not considered.

394 Fig. 13 displays near-wall profiles for temperature fluctuations and total (resolved +

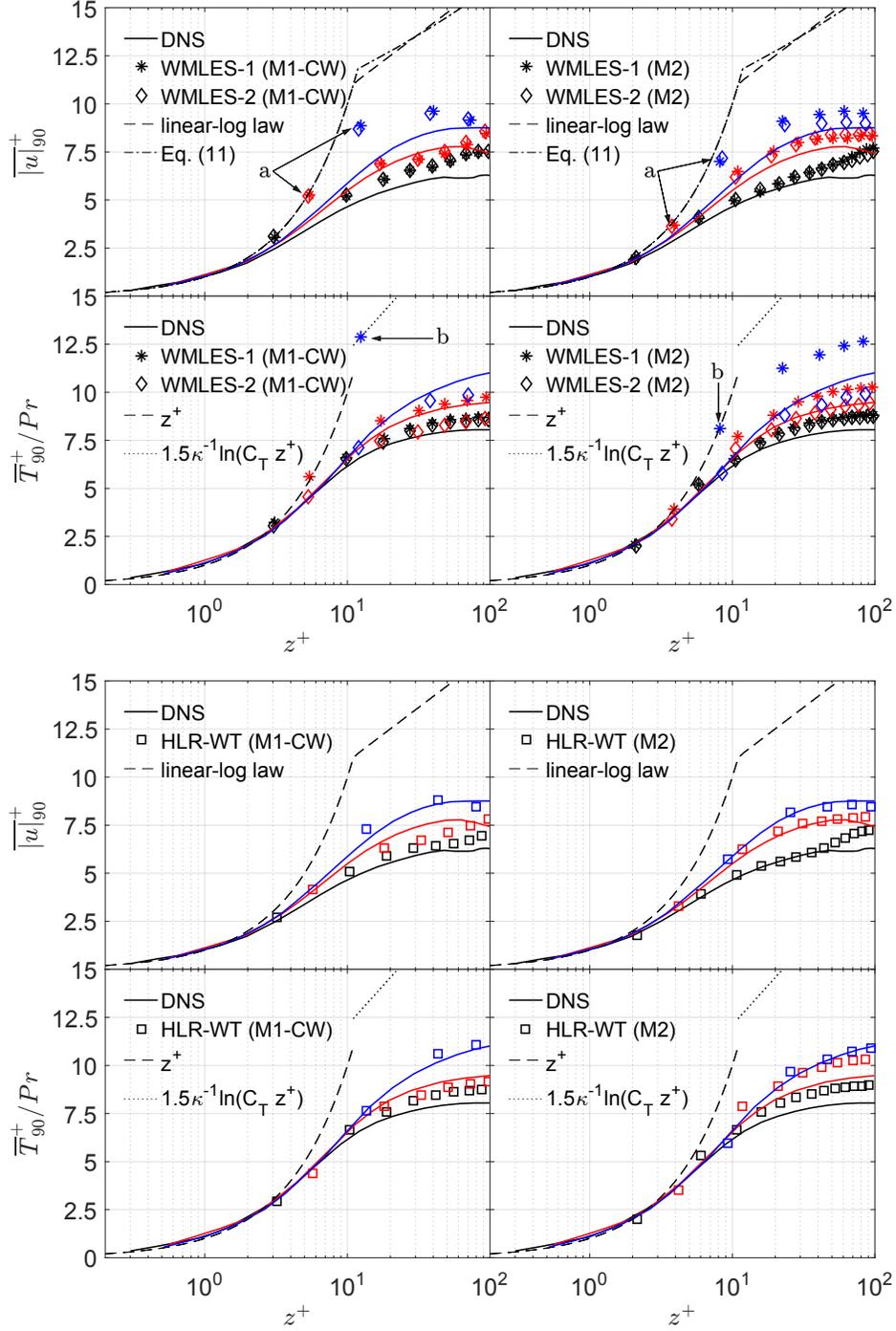


Figure 12: Stage III: scaled near-wall mean profiles of velocity magnitude (top frames) and temperature (bottom frames) at 270°C (black), 306°C (red) and 346°C (blue). WMLES-methods (top) and HLR-WT (bottom) with coarse (M1-CW, left) and intermediate (M2, right) grids. Variables are scaled as $z^+ = (z/\nu_w)\bar{u}_{\tau 90}$, $|u|^+ = |u|/\bar{u}_{\tau 90}$, $T^+ = (T_w - T)\rho_w c_{p,w}\bar{u}_{\tau 90}/q_{w 90}$.

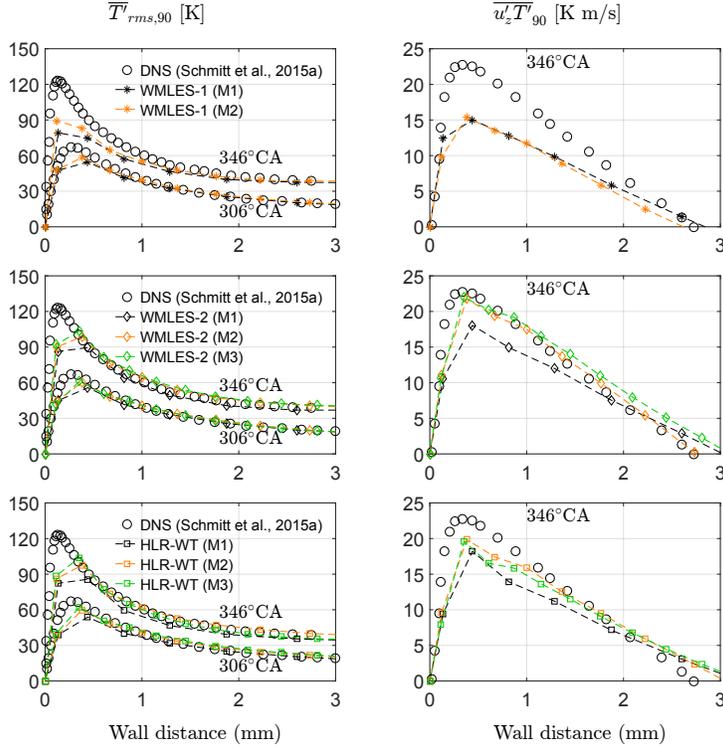


Figure 13: Stage III, cycle A: cylinder head near-wall profiles of rms temperature fluctuations (centre) and total (resolved + modelled) turbulent heat flux (right). WMLES-1 (top), WMLES-2 (centre) and HLR-WT (bottom) approaches.

395 modelled) turbulent heat flux. While differences in $\overline{T'}_{rms}$ are minute at 306°CA, the later
 396 timing of 346°CA shows greater result variation. Core grid refinement improves both $\overline{T'}_{rms}$
 397 and turbulent heat flux profiles – however, the high near-wall $\overline{T'}_{rms}$ peak in the DNS is not
 398 accurately captured with any of the present computations. In comparison to WMLES-1,
 399 WMLES-2 and HLR-WT cases yield improved fluctuation profiles. In correspondence with
 400 the results in Table 3, CW grid results (not shown here for brevity) produce a more substantial
 401 underprediction of the fluctuations.

402 3.6. Local metrics and the wall heat transfer mechanism

403 Fig. 14 illustrates instantaneous wall heat flux distributions on the cylinder head ($z = 0$)
 404 surface at 306°CA and 360°CA. In addition, PDFs for the heat transfer coefficient $\alpha =$
 405 $q_w / (\overline{T}_V - T_W)$ are shown for the TDC time instance. As noted by Schmitt et al. (2016b),
 406 the prevalent local regions of high heat flux are primarily due to wall-impinging hot streams.
 407 The turbulent scales reduce substantially during compression due to the dramatic decrease
 408 in kinematic viscosity, particularly close to the (relatively cold) wall. At 306°CA, the dif-

409 ferent models yield relatively similar distributions that coincide qualitatively with the DNS,
410 although a clear difference in the resolved scales is already visible. Such a result similarity
411 corresponds to the near-wall profiles in Figs. 12 and 13 – indeed, at 306°CA the wall-adjacent
412 M2 grid node is still within the viscous sublayer ($y_1^+ \approx 4$).

413 TDC conditions, resulting in minuscule scales and vast local variations in the DNS fields,
414 offer considerably different results. While near-wall scales have evidently reduced in the
415 wall-modelled computations, the smallest structures found in the DNS are far beyond the
416 reach of the present grids. Hence, comparison is additionally carried out with DNS data box-
417 filtered onto the M2 surface grid (FDNS), representing a more feasible point of reference for
418 the wall-modelled methods (Yang et al., 2017). Such filtering effectively results in a slightly
419 narrower heat transfer coefficient PDF. While the present wall-modelled heat transfer distri-
420 butions expectedly correspond better with the FDNS than with the DNS, result differences
421 are not entirely mitigated for any of the present computations. With the M2 grid, WMLES-1
422 shows the smallest local variations, as evidenced also by the narrow, high-peak shape of the
423 corresponding PDF. Comparing WMLES-2 and HLR-WT (with approximately similar mean
424 values), the latter displays finer structures with higher local maxima and slightly improved
425 α correspondence against the DNS. Such differences indicate that there are differences as to
426 how the peaks are formed (to be discussed later).

427 With the M2-CW grid, the differences between M2 observations appear to have increased
428 further. While mean values remain relatively similar with WMLES-2 and HLR-WT, the
429 replication of local heat transfer variation has clearly deteriorated. For rationale thereto,
430 we can refer to the wall-normal spacing relative to the boundary layer thickness δ_{90} (Fig.
431 3). Close to TDC, the CW spacing gradually approaches δ_{90} , posing a suboptimal situation
432 from the perspective of wall modelling: Larsson et al. (2016) state an optimal wall-modelled
433 layer to be ca. 20% of the boundary layer thickness. It is not immediately apparent how
434 such criteria should be formed for the characteristically specific in-cylinder flows. It should
435 however be noted that wall-modelled scale-resolving simulations are not generally known for
436 high-quality wall flux fluctuation predictions (Yang et al., 2017).

437 As the local heat flux distributions in Fig. 14 cannot indicate wall-normal convection,

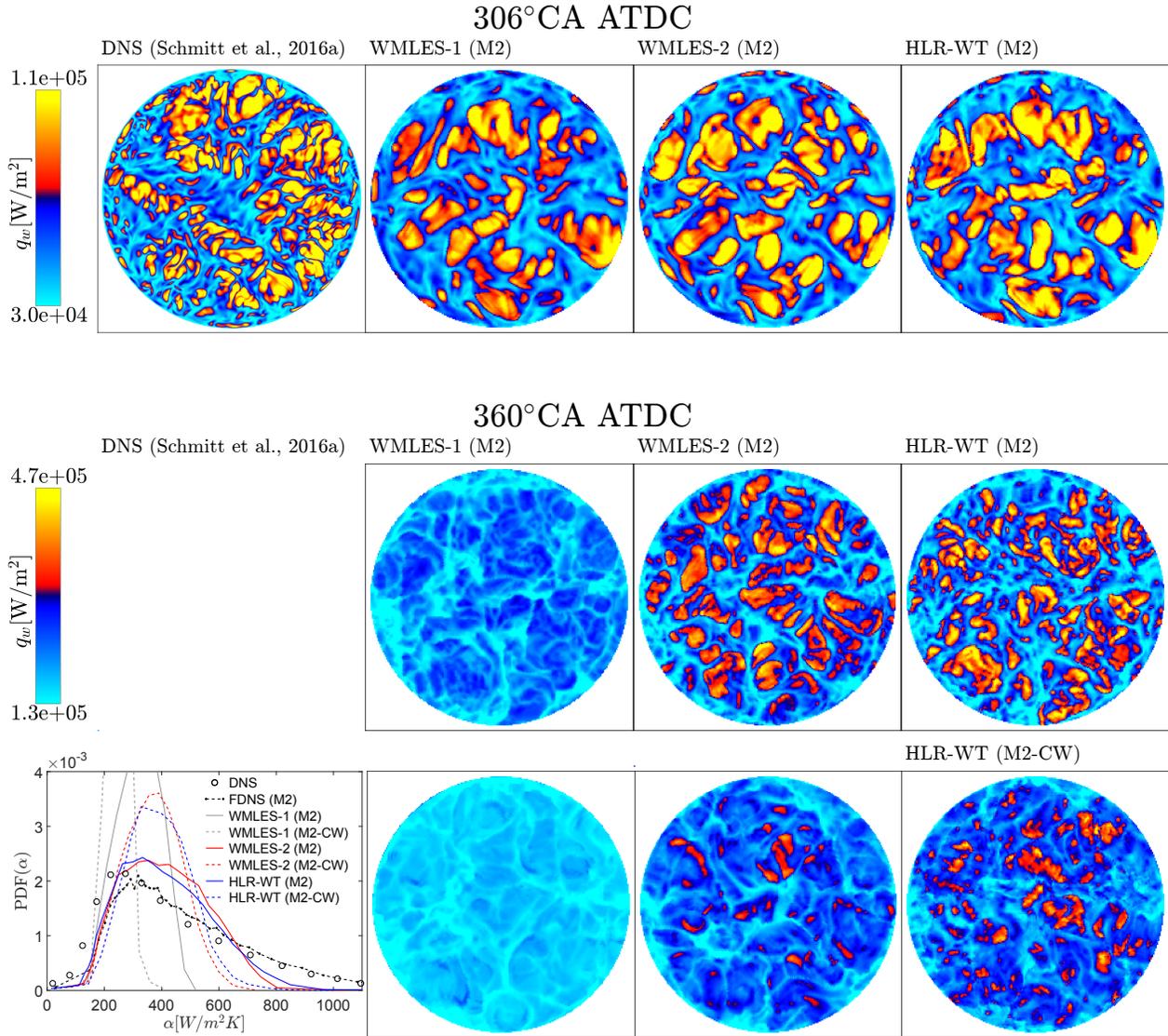


Figure 14: Stage III, cycle A: instantaneous cylinder head heat transfer rate depicted at 306°CA (top) and at TDC (bottom). For TDC, distributions are shown with both M2 and M2-CW grids. Due to the high difference in resolved scales between the DNS and the present simulations at TDC, a filtered DNS distribution (FDNS [M2]) is additionally displayed. Alongside the images, heat transfer coefficient PDFs over all cylinder walls are illustrated.

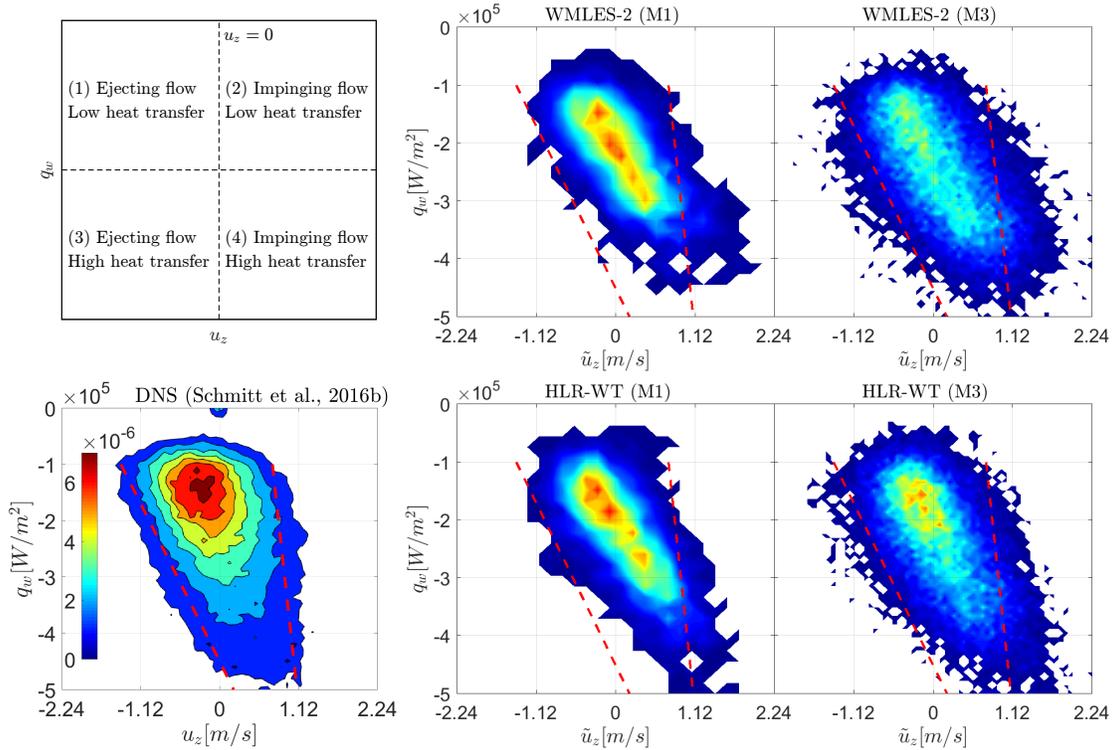


Figure 15: Stage III, cycle A: joint PDFs of wall-normal velocity at $z = -0.9375$ mm and wall heat flux at the corresponding wall location at 346°CA . The reference DNS (bottom left) is shown alongside WMLES-2 (top right) and HLR-WT (bottom right) computations with differing core grid resolutions. Red dashed guide lines (adopted from the DNS trends) are identical in each frame.

438 instrumental to the wall heat transfer mechanism of impinging ($u_z > 0$) and ejecting ($u_z < 0$)
 439 streams (Schmitt et al., 2016b), additional insight is sought by correlating the wall heat flux
 440 with the adjacent flow field. Fig. 15 presents joint PDFs of u_z and q_w for WMLES-2 and HLR-
 441 WT across the cylinder head surface and illustrates conceptual interpretations of different
 442 PDF regions. The diagonally oriented distributions signify the high contribution of flow
 443 types 1 (ejecting with low heat transfer) and 4 (impinging with high heat transfer). Hence,
 444 the heat transfer mechanism observed in the DNS appears to be qualitatively replicated. In
 445 comparison to the DNS, type 4 flows are slightly overrepresented, and the distributions are
 446 more tilted. With HLR-WT, both grids suggests a minor improvement over the corresponding
 447 WMLES-2 case.

448 3.7. Model functionality in different flow zones

449 In order to more closely inspect the minute differences in local near-wall metrics observed
 450 between WMLES-2 and HLR-WT, model functionality is examined in different local flow

451 regions. The present wall-modelled simulations cannot evidently be expected to accurately
 452 reproduce the small-scale flow physics in the near-wall region. However, a filtered DNS
 453 distribution may be used to illustrate how heat transfer models should respond to ejecting
 454 and impinging flows on a larger scale.

455 Fig. 16 displays the scaled heat flux $q_w/\overline{q_{w90}}$ and is overlaid with the wall shear stress
 456 field. With both WMLES-2 and HLR-WT, ejection locations can be identified by near-wall
 457 counterflow with low local heat transfer, consistent with expectations from the FDNS. For
 458 impinging flow, heat flux maxima should be expected at stagnation regions. With WMLES-
 459 2, such local maxima are largely absent: instead, highest heat transfer values are generally
 460 located where the flow is tangential. Indeed, this property, resulting from the strong depen-
 461 dence between q_w and u_τ (Eq. 14), was acknowledged by Plensgaard (2013). An improved
 462 representation of stagnation regions is noted with HLR-WT, where the link between τ_w and
 463 q_w is considerably weaker than in the algebraic models. The plots in Fig. 16 demonstrate
 464 how the local differences occur by applying WMLES-2 instantaneously on the HLR-WT
 465 field in wall-adjacent locations A, B and C. Approximately similar predictions are noted
 466 in ejecting (A) and tangential (B) locations (where a correlation between τ_w and q_w is ex-
 467 pected) while a large difference is noted in the impinging flow (C). Here, the combination
 468 of a low u_τ value and high temperature difference results in only a moderate heat flux with
 469 WMLES-2. In contrast, the HLR-WT profile is considerably influenced by the imbalance
 470 term $I_h = (q_h - q_w)/\Delta y$ within the solution of Eq. (16), increasing the near-wall gradient.
 471 Effectively, the utilisation of two near-wall main grid points in the model of Nuutinen et al.
 472 (2014) permits the incorporation of an additional piece of information on the local flow state.

473 3.8. Influence of the HLR-WT non-equilibrium model

474 As detailed in Sec. 2.4.2, the HLR-WT wall treatment solves simplified 1-D TBLEs
 475 with a non-equilibrium model that incorporates values of variables at both first and second
 476 wall-adjacent cell centres. To specifically illustrate how the non-equilibrium model influences
 477 results, we modify the HLR-WT approach so that imbalance terms are cancelled within the
 478 iterative routine, i.e. $I_m = I_h = 0$ in Eqs. (15) and (16). This reduces the approach to a
 479 1-D equilibrium model (HLR-WT-EQ) and omits the influence of the second near-wall grid

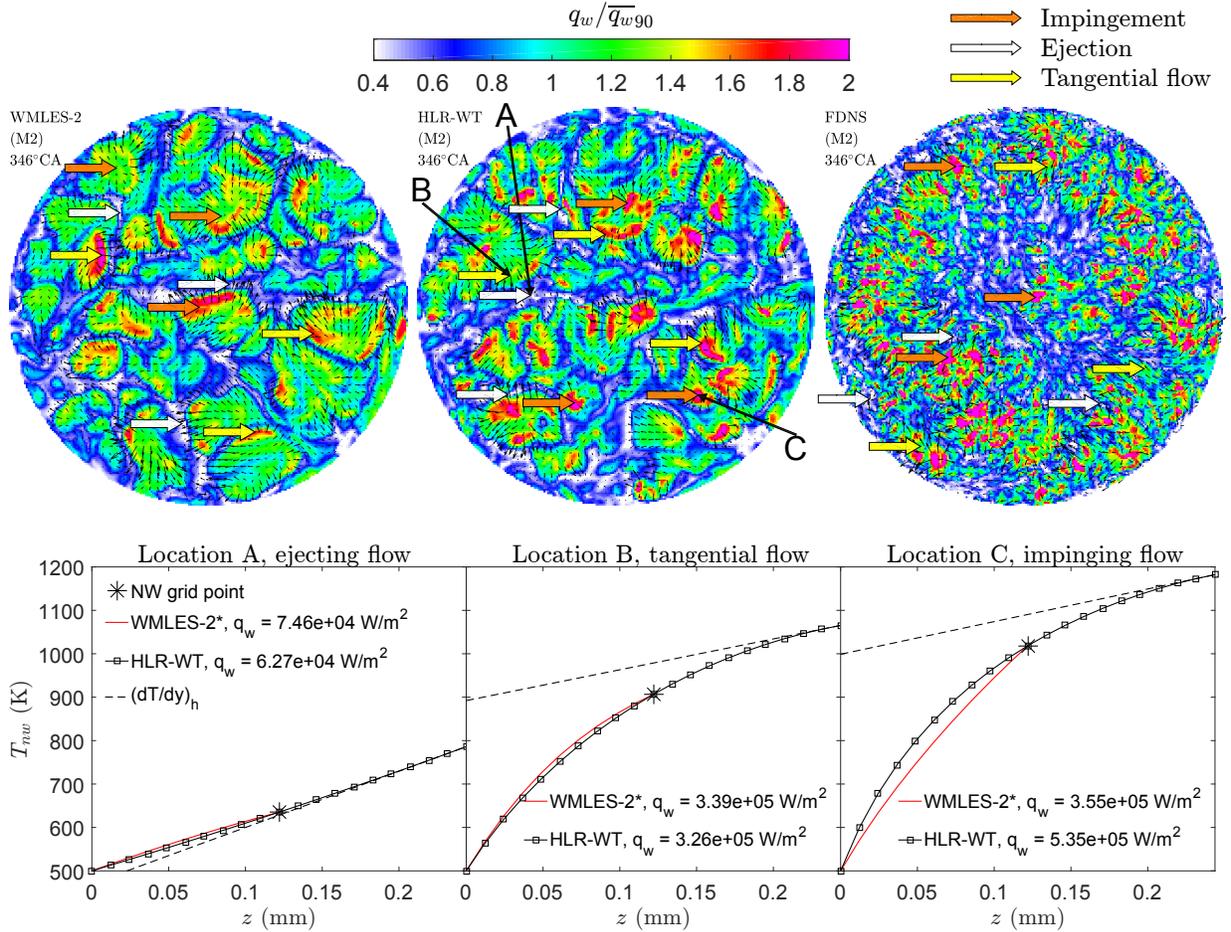


Figure 16: Stage III, cycle A. Top: normalised instantaneous cylinder head heat flux distribution $q_w/\overline{q_{w90}}$ overlaid with wall shear stress vectors at 346°CA with WMLES-2 (left) and HLR-WT (centre) approaches. Filtered DNS fields are shown as a reference (right). Arrows exemplify locations of impingement (orange), ejection (white) and tangential flow (yellow). Bottom: illustration of instantaneous wall model predictions throughout the near-wall cell in different flow types. In addition to the HLR-WT subgrid solution and the algebraic WMLES-2 profile, dashed lines denote the temperature gradient determined by q_h , which functions as a boundary condition in HLR-WT. The superscript (*) denotes that the WMLES-2 wall model is instantaneously applied on the HLR-WT field.

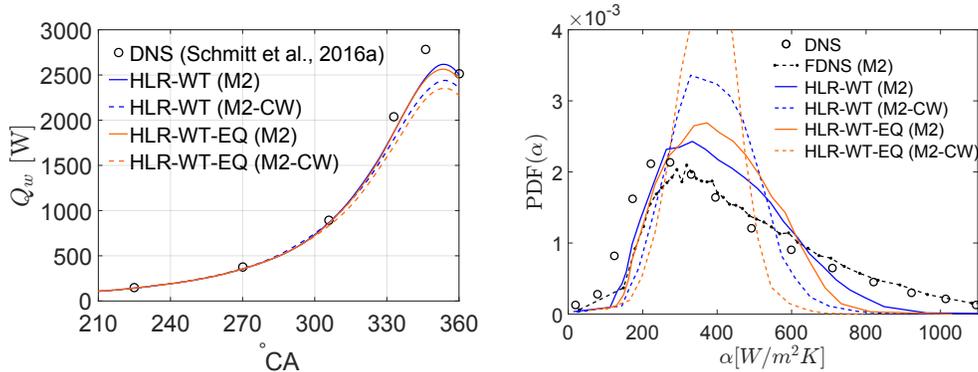


Figure 17: Stage III, cycle A. Heat transfer comparison between HLR-WT and its equilibrium modification (HLR-WT-EQ). Total wall heat transfer rate throughout compression (left) and wall heat transfer coefficient PDF at TDC (right).

480 point. Fig. 17 displays the resulting effects in terms of total wall heat transfer and heat flux
 481 fluctuations with the M2 and M2-CW grids. In terms of total heat flux, the non-equilibrium
 482 model results in a mild improvement which is more pronounced in the case of the coarse
 483 near-wall grid. The wall heat transfer coefficient PDFs differ more clearly: use of the non-
 484 equilibrium model results in higher contributions of both low and high heat transfer extrema,
 485 in better correspondence with the DNS. These observations indicate that the non-equilibrium
 486 model yields clear result benefits in the HLR-WT approach.

487 3.9. Discussion

488 With the present wall-modelled cases, computational cost scales relatively leniently when
 489 core grid resolution is increased: as both near-wall and core grid scales are not highly detached
 490 (Table 2), additional time step restrictions remain mild. This is in strong contrast to wall-
 491 resolved LES and even wall normal-resolved hybrid methods, where significant bottlenecks
 492 may arise. Unlike increases in cell count which can be managed with increased parallelisation
 493 in the case of highly scalable codes, temporal parallelisation cannot be similarly incorporated
 494 (Larsson and Wang, 2014). Hence, a large number of time steps considerably influences
 495 simulation turnaround time.

496 The simplicity and low computational cost of algebraic models is an attractive aspect in
 497 comparison to 1-D methods. The fair performance of WMLES-2 in the present work encour-
 498 ages further investigation of such models. The DNS revealed that semi-local scaling (em-
 499 ploying local material properties) results in increased similarity between the nondimensional

500 boundary layer profiles (Schmitt et al., 2015a), offering one possible development pathway.
501 Novel compressible flow formulations analogous to the Van Driest transformation (e.g. Trettel
502 and Larsson, 2016) can also be incorporated. Still, the most challenging hurdle for algebraic
503 models may be induced by the fundamental complexity of ICE boundary layers, highlighted
504 in other contemporary modelling-related studies (Ma et al., 2017a; Renaud et al., 2018).

505 It needs to be noted that ICE flows entail a much broader scope than what the present,
506 highly simplified configuration represents. In addition to the influence of engine speed, co-
507 herent charge motions such as swirl, tumble or squish flows are routinely present in real
508 ICE configurations and are expected to influence the scaled profiles and the functionality of
509 wall models. Indeed, further wall-modelled investigations of well-documented non-reacting
510 engine configurations could provide valuable additional insight to complement the present
511 work. Moreover, wall modelling for high Reynolds number reacting flows, outside of the
512 scope of the present work, is a highly challenging and emerging research area. Thereby, the
513 results of the present study certainly pose some limitations and their projection to the real
514 engine context may not be completely straightforward.

515 **4. Summary and conclusions**

516 Wall-modelled scale-resolving simulations were carried out in engine-like flows using DNS
517 data as a reference. The computations involved three consecutive stages, namely (I) a multi-
518 cycle cold flow process, (II) fuel-air intake, and (III) charge compression. Stages I and II were
519 first assessed with the HLR-WT model, yielding an acceptable match to the reference DNS.
520 Stage III, the study focus, comprised assessment of two algebraic wall models (WMLES-1,
521 WMLES-2) and a 1-D subgrid-based approach (HLR-WT). Grids differing in both off-wall
522 and near-wall resolution were investigated.

523 In the compression stroke it was found that WMLES-1, utilising standard wall laws, led
524 to a substantial and highly grid dependent underprediction of wall heat transfer and thermal
525 fluctuations. WMLES-2 and HLR-WT, entailing wall models developed in the context of
526 engine flows, delivered considerably improved predictions of volume-averaged thermal metrics
527 with lower grid sensitivity.

528 Scaled near-wall profiles indicated that all approaches yielded acceptable results when the
529 near-wall grid point was within the viscous sublayer. Outside of the sublayer, wall shear stress
530 was underpredicted with the algebraic models due to their relatively close adherence with
531 the Werner-Wengle power law. WMLES-1 continued a similar trend with thermal scaling,
532 explaining the near-wall grid sensitivity in thermal predictions. In contrast, the engine-
533 targeted WMLES-2 (based on the model of Han and Reitz (1997)) provided considerably
534 improved thermal scaling. For all grids tested in this work, HLR-WT resulted in fairly
535 appropriate scaling throughout the compression stroke for both momentum and thermal
536 boundary layers.

537 With WMLES-2 and HLR-WT, closer inspection of near-wall processes indicated a qual-
538 itative replication of the near-wall impingement-ejection process observed in the DNS. The
539 present grids and methods were however not able to fully capture the wall heat transfer
540 fluctuations. In the present configuration, HLR-WT provided a slight enhancement in the
541 reproduction of such fluctuations and an improved description of heat transfer maxima asso-
542 ciated with impinging streams. Comparison with an equilibrium modification of HLR-WT
543 indicated that the non-equilibrium model improved heat transfer predictions.

544 Core grid refinement generally improved the fidelity of near-wall fluctuating metrics and
545 the impingement-ejection process. In contrast, use of coarse near-wall grids in the wall-
546 normal direction resulted in a substantial deterioration of such fidelity with all models. The
547 results provide evidence of the potential of the HLR-WT and WMLES-2 approaches for
548 the prediction of near-wall ICE processes. While further charge formation patterns and
549 engine conditions with differing near-wall profiles should be tested for a more comprehensive
550 understanding, the reported observations augment the recent notions (Ma et al., 2017a,b)
551 that advanced near-wall models may offer benefits for in-cylinder flow and heat transfer
552 simulations.

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Appendix A. 1-D non-equilibrium model implementation

Fig. A.18 displays the structural schematic of the near-wall model while Fig. A.19 describes model workflow between the main grid and the near-wall subgrid. Following Fig. A.18, the wall-tangential flow direction is determined from the main grid solution and the local x -axis is set to be parallel to this velocity. Subscripts w , c , h , and $2c$ henceforth correspond to wall, first cell centre, cell face, and second cell centre values, respectively, while filtering notations in addition to modelled k and ε subscripts are dismissed for clarity. The cell face quantities $\tau_h = ([\mu + \mu_{mod}]du/dy)_h$ and $q_h = (c_p[\mu/Pr + \mu_{mod}/Pr_{mod}]dT/dy)_h$ are evaluated from the main grid data. After initialisation of τ_w and q_w , (e.g. via standard wall functions), variables are scaled as follows:

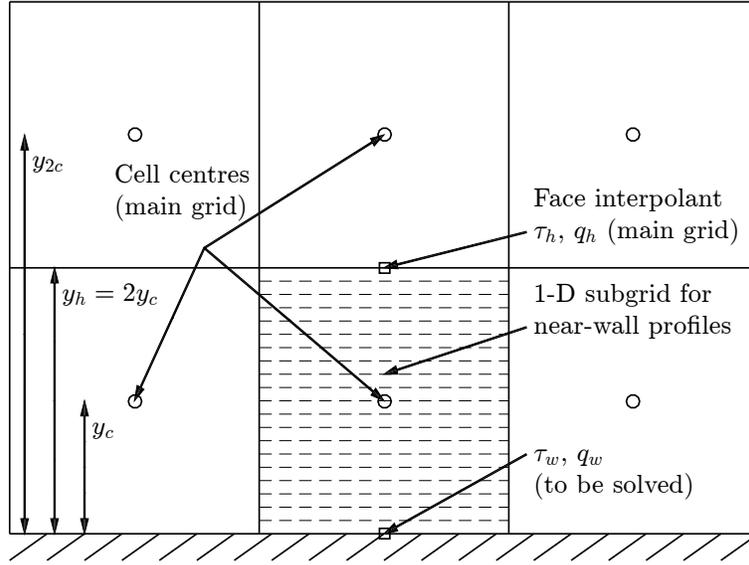


Figure A.18: A schematic description of the wall treatment applied here (HLR-WT) and first published by Nuutinen et al. (2014). Subscripts w , c , h , and $2c$ correspond to wall, first cell centre, cell face, and second cell centre values, respectively.

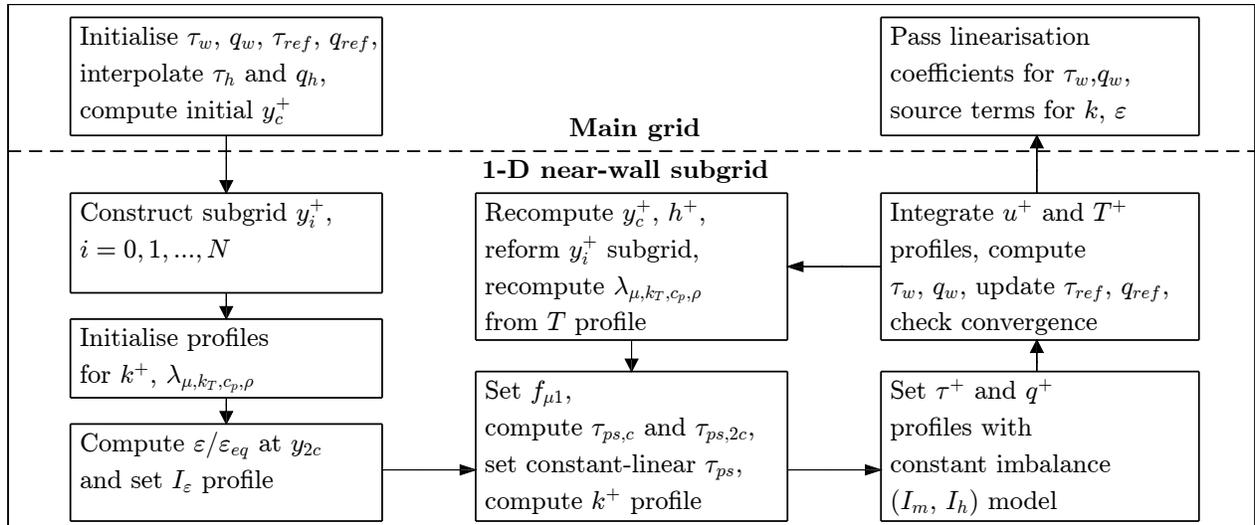


Figure A.19: Workflow chart of the wall treatment between the main grid and the 1-D subgrid.

$$\begin{aligned}
y^+ &= \rho_c u_\tau y / \mu_c & (\rho\varepsilon)^+ &= \rho\varepsilon / (\rho_c^2 u_\tau^4 / \mu_c) & k^+ &= C_\mu k^{1/2} / u_\tau^2 \\
u^+ &= (u - u_w) / u_\tau & T^+ &= \rho_c c_{p,c} u_\tau (T - T_w) / q_w & \tau^+ &= \tau_w / \tau_{ref} \\
q^+ &= q_w / q_{ref}
\end{aligned} \tag{A.1}$$

where the shear velocity $u_\tau = (\tau_{ref} / \rho_c)^{1/2}$ and the 'reference' wall shear stress and heat flux values ($\tau_{ref} = \tau_w + \tau_{small}$, $q_{ref} = q_w + q_{small}$) have been introduced to avoid zero division. The initial subgrid y_i^+ ($i = 0, 1, \dots, N$) is then constructed. To describe subgrid material property variation, scaled profiles λ_μ , λ_{k_T} , λ_{c_p} , λ_ρ denote μ/μ_c , $k_T/k_{T,c}$, $c_p/c_{p,c}$ and ρ/ρ_c , respectively. The profiles are approximated with power laws, e.g. for viscosity:

$$\lambda_\mu = \frac{\mu}{\mu_c} = \left(\frac{T}{T_c} \right)^\Phi \tag{A.2}$$

wherein the exponent is obtained from the reference values, i.e. $\Phi = \ln(\mu_w/\mu_c) / \ln(T_w/T_c)$. The reference values (at cell centres and walls) are computed by Star-CD internally using more complex models. The power law exponents are estimated similarly for other quantities, with the exception of density, where $\Phi = -1$ due to the ideal gas law.

After initialising $\lambda_{\mu,k_T,c_p,\rho} = 1$, a dissipation rate imbalance profile I_ε is computed according to a linear profile between $I_{\varepsilon,w} = 1$ and $I_{\varepsilon,2c} = \varepsilon(y_{2c}) / \varepsilon_{eq}(y_{2c})$. Here, $\varepsilon = (\varepsilon_{iso} + \varepsilon_{wall}) I_\varepsilon$ where isotropic dissipation $\varepsilon_{iso} = C_\mu^{3/4} k^{3/2} / (\kappa y)$, wall dissipation $\varepsilon_{wall} = 2\nu(k/y^2)g_\varepsilon$ and $\varepsilon_{eq} = \varepsilon_{iso} + \varepsilon_{wall}$ is the equilibrium form. The shape function $g_\varepsilon = 1 - (y^*/\delta_\varepsilon) \exp(-\chi_\varepsilon y^*/2\delta_\varepsilon)$ (where $\delta_\varepsilon = 3.31$, $\chi_\varepsilon = 0.75$, $y^* = \rho C_\mu^{1/4} k(y/\mu)$) is set to cancel near-wall diffusion of k (exactly at the wall). The damping function profile is computed nondimensionally as $f_{\mu 1}^+ = 1 - \beta_\mu \exp(-\alpha_\mu [\lambda_\rho / \lambda_\mu] k^{+1/2} y^+)$. $\beta_\mu = 1 - (\rho\varepsilon)_w^+ C_\mu^{1/2} / (2\kappa^2) = 0.7864$ has been calibrated for a realistic (non-zero) wall dissipation level $(\rho\varepsilon)_w^+ = 0.25$ on the basis of DNS studies (Iwamoto et al., 2002a,b) while $\alpha_\mu = 0.011857$ is set to asymptotically match standard wall functions in ideal conditions. A corrected k^+ profile is generated utilising a pseudo-stress τ_{ps}

$$\tau_{ps} = \frac{I_\varepsilon C_\mu^{1/4} k^{1/2} (\mu + \mu_{mod})}{\kappa y f_{\mu 1}^{1/2}} \tag{A.3}$$

whereby a constant value $\tau_{ps,c}$ is set for the interval $y = [0, y_c]$ while a linear variation from

$\tau_{ps,c}$ to $\tau_{ps,h}$ (based on $\tau_{ps,2c}$) is set between $y = [y_c, y_h]$. Thereafter, an updated k^+ profile is computed

$$k^+ = \left(\frac{2\kappa y^+ f_{\mu 1}^{+1/2} \tau_{ps}^+ / I_\varepsilon}{\lambda_\mu + [\lambda_\mu^2 + 4\lambda_\rho \kappa^2 y^{+2} f_{\mu 1}^{+3/2} \tau_{ps}^+ / I_\varepsilon]^{1/2}} \right)^2 \quad (\text{A.4})$$

where $\tau_{ps}^+ = \tau_{ps} / \tau_{ref}$. Eqs. (15)-(16) are expressed nondimensionally as

$$\frac{du^+}{dy^+} = \frac{\tau^+}{\lambda_\mu + \lambda_\rho \kappa y^+ k^{+1/2} f_{\mu 1}^+ / I_\varepsilon} \quad (\text{A.5})$$

$$\frac{dT^+}{dy^+} = \frac{Pr_c Pr_{mod} q^+}{Pr_{mod} \lambda_{k_T} + Pr_c \lambda_{c_p} \lambda_\rho \kappa y^+ k^{+1/2} f_{\mu 1}^+ / I_\varepsilon} \quad (\text{A.6})$$

where the modelled Prandtl number $Pr_{mod} = 0.9 (1 - \exp[-\gamma \sqrt{y^+}])$ and $\gamma = 0.9470$. Eqs. (A.5) and (A.6) are numerically integrated to yield the velocity and temperature profiles – here, scaled τ^+ and q^+ profiles are linear similarly to Eqs. (15) and (16):

$$\tau^+ = \frac{\tau_w + (\tau_h - \tau_w)(y^+ / h^+)}{\tau_{ref}} \quad q^+ = \frac{q_w + (q_h - q_w)(y^+ / h^+)}{q_{ref}} \quad (\text{A.7})$$

Finally, wall fluxes are computed for the next iterative step $n + 1$ (or, after convergence of u^+ and T^+ , to the main grid) in linearised form as

$$\tau_w^{n+1} = \overbrace{\left(\left[\begin{array}{c} \tau_w \\ \tau_{ref} \end{array} \right] \left[\begin{array}{c} y_c^+ \\ u_c^+ \end{array} \right] \right)}^{lin.coeff.} \left(\frac{\mu_c}{y_c} \right) (u_c - u_w) \quad (\text{A.8})$$

$$q_w^{n+1} = \overbrace{\left(\left[\begin{array}{c} q_w \\ q_{ref} \end{array} \right] \left[\begin{array}{c} y_c^+ \\ T_c^+ \end{array} \right] \right)}^{lin.coeff.} \left(\frac{c_{p,c} \mu_c}{y_c} \right) (T_c - T_w) \quad (\text{A.9})$$

For the next iterative step, updated material properties are computed based on the temperature profile, while the subgrid y_i^+ is modified based on the updated wall shear stress value. Modelled turbulence source terms are provided as

$$\langle \rho P_k \rangle = \langle \rho P_{k,tan}^{nw} \rangle + (\rho P_k^{main} - \rho P_{k,tan}^{main}) \quad (\text{A.10})$$

$$\langle \rho \varepsilon \rangle = \frac{\langle (\rho \varepsilon)^+ \rangle}{(\rho \varepsilon)_c^+} \varepsilon_{eq,c} I_{\varepsilon,c} \quad (\text{A.11})$$

where angled brackets denote averaging over the near-wall subgrid. The near-wall tangential production is obtained as

$$\langle \rho P_{k,tan}^{nw} \rangle = \left\langle \lambda_\rho \kappa y^+ k^{+1/2} f_{\mu_1}^+ (du^+ / dy^+)^2 / I_\varepsilon \right\rangle (\rho_c^2 u_\tau^4 / \mu_c) \quad (\text{A.12})$$

Appendix B. Preliminary cycle selection criteria

From the results of Stage I computations, a nominal cycle (A) is determined in addition to two differing cycles (B and C). Cycles are determined based on mean axial flow profiles at 90°CA ATDC (Fig. 5) so that A is the cycle closest to the mean statistical cycle, B is farthest from A, and C is farthest from B. This procedure utilises the following metric:

$$M_{cn} = \sum_i \sum_j \left| r_j \left(\langle \tilde{u}_z(r_j, z_i) \rangle_{\phi, cn} - u_{z,ref} \right) \right| \quad (\text{B.1})$$

where cn is the cycle number and $\langle \cdot \rangle_{\phi, cn}$ signifies instantaneous azimuthal averaging within the selected cycle. Summation is carried out over equally spaced radial points r_j located at axial planes $z_i = [-10, -20, \dots, -50]$ mm and $u_{z,ref}$ is a reference profile set. Profile differences are radially weighted to ensure equivalence in axial momentum contribution.

For the determination of nominal cycle A, a minimum of M_{cn} is probed with respect to the statistical mean cycle ($u_{z,ref} = \langle \tilde{u}_z \rangle$ where $\langle \cdot \rangle$ denotes averaging over both the azimuthal coordinate and all of the 17 considered cycles). For cycle B, a maximum of M_{cn} is sought with the azimuthally averaged cycle A as the reference ($u_{z,ref} = \langle \tilde{u}_z \rangle_{\phi, A}$) whereas for determining cycle C, a maximum of M_{cn} is determined with cycle B as the reference.